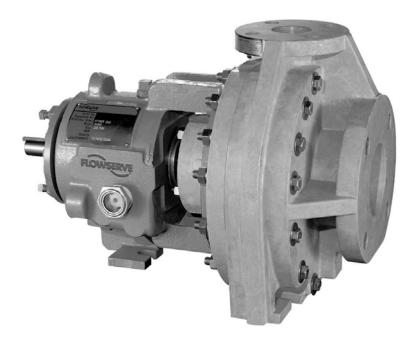


Pump Division



PolyChem GRP Pumps ANSI B73.5M Standard Horizontal And Self-Priming Non-metallic, Frame-mounted

USER INSTRUCTIONS: INSTALLATION, OPERATION, MAINTENANCE

PCN = 71569132 - 12/04 (E)

These instructions must be read prior to installing, operating, using and maintaining this equipment.



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1 INTRODUCTION AND SAFETY

1.1 General

These instructions must always be kept close to the product's operating location or directly with the product.

Flowserve's products are designed, developed and manufactured with state-of-the-art technologies in modern facilities. The unit is produced with great care and commitment to continuous quality control, utilizing sophisticated quality techniques, and safety requirements.

Flowserve is committed to continuous quality improvement and being at your service for any further information about the product in its installation and operation or about its support products, repair and diagnostic services.

These instructions are intended to facilitate familiarization with the product and its permitted use. Operating the product in compliance with these instructions is important to help ensure reliability in service and avoid risks. The instructions may not take into account local regulations; ensure such regulations are observed by all, including those installing the product. Always coordinate repair activity with operations personnel, and follow all plant safety requirements and applicable safety and health laws/ regulations.

These instructions must be read prior to installing, operating, using and maintaining the equipment in any region worldwide. The equipment must not be put into service until all the conditions relating to safety noted in the instructions, have been met.

1.2 CE marking and approvals

It is a legal requirement that machinery and equipment put into service within certain regions of the world shall conform with the applicable CE Marking Directives covering Machinery and, where applicable, Low Voltage Equipment, Electromagnetic Compatibility (EMC), Pressure Equipment Directive (PED) and Equipment for Potentially Explosive Atmospheres (ATEX).

Where applicable, the Directives and any additional Approvals, cover important safety aspects relating to machinery and equipment and the satisfactory provision of technical documents and safety instructions. Where applicable this document incorporates information relevant to these Directives and Approvals. To confirm the Approvals applying and if the product is CE marked, check the serial number plate markings and the Certification, see section 9, *Certification*.

1.3 Disclaimer

Information in these User Instructions is believed to be reliable. In spite of all the efforts of Flowserve Pump Division to provide sound and all necessary information the content of this manual may appear insufficient and is not guaranteed by Flowserve as to its completeness or accuracy.

Flowserve manufactures products to exacting International Quality Management System Standards as certified and audited by external Quality Assurance organizations. Genuine parts and accessories have been designed, tested and incorporated into the products to help ensure their continued product quality and performance in use. As Flowserve cannot test parts and accessories sourced from other vendors the incorrect incorporation of such parts and accessories may adversely affect the performance and safety features of the products. The failure to properly select, install or use authorized Flowserve parts and accessories is considered to be misuse. Damage or failure caused by misuse is not covered by Flowserve's warranty. In addition, any modification of Flowserve products or removal of original components may impair the safety of these products in their use.

1.4 Copyright

All rights reserved. No part of these instructions may be reproduced, stored in a retrieval system or transmitted in any form or by any means without prior permission of Flowserve Pump Division.

1.5 Duty conditions

This product has been selected to meet the specifications of your purchaser order. The acknowledgement of these conditions has been sent separately to the Purchaser. A copy should be kept with these instructions.

The product must not be operated beyond the parameters specified for the application. If there is any doubt as to the suitability of the product for the application intended, contact Flowserve for advice, quoting the serial number.



If the conditions of service on your purchase order are going to be changed (for example liquid pumped, temperature or duty) it is requested that the user seeks Flowserve's written agreement before start up.

1.6 Safety

1.6.1 Summary of safety markings

These User Instructions contain specific safety markings where non-observance of an instruction would cause hazards. The specific safety markings are:

DANGER This symbol indicates electrical safety instructions where non-compliance will involve a high risk to personal safety or the loss of life.

This symbol indicates safety instructions where non-compliance would affect personal safety and could result in loss of life.

This symbol indicates "hazardous and toxic fluid" safety instructions where non-compliance would affect personal safety and could result in loss of life.

This symbol indicates safety instructions where non-compliance will involve some risk to safe operation and personal safety and would damage the equipment or property.

This symbol indicates explosive atmosphere zone marking according to ATEX. It is used in safety instructions where non-compliance in the hazardous area would cause the risk of an explosion.

Note: This sign is not a safety symbol but indicates an important instruction in the assembly process.

1.6.2 Personnel qualification and training

All personnel involved in the operation, installation, inspection and maintenance of the unit must be qualified to carry out the work involved. If the personnel in question do not already possess the necessary knowledge and skill, appropriate training and instruction must be provided. If required the operator may commission the manufacturer/supplier to provide applicable training.

Always coordinate repair activity with operations and health and safety personnel, and follow all plant safety requirements and applicable safety and health laws and regulations.

1.6.3 Safety action

This is a summary of conditions and actions to prevent injury to personnel and damage to the environment and to equipment. For products used in potentially explosive atmospheres section 1.6.4 also applies.

DANGER NEVER DO MAINTENANCE WORK WHEN THE UNIT IS CONNECTED TO POWER (Lock Out)

DRAIN THE PUMP AND ISOLATE PIPEWORK BEFORE DISMANTLING THE PUMP The appropriate safety precautions should be taken where the pumped liquids are hazardous.

FLUOROELASTOMERS (When fitted.) When a pump has experienced temperatures over 250 °C (482 °F), partial decomposition of fluoroelastomers (example: Viton) will occur. In this condition these are extremely dangerous and skin contact must be avoided.

A HANDLING COMPONENTS

Many precision parts have sharp corners and the wearing of appropriate safety gloves and equipment is required when handling these components. To lift heavy pieces above 25 kg (55 lb) use a crane appropriate for the mass and in accordance with current local regulations.

NEVER OPERATE THE PUMP WITHOUT THE COUPLING GUARD AND ALL OTHER SAFETY DEVICES CORRECTLY INSTALLED

GUARDS MUST NOT BE REMOVED WHILE THE PUMP IS OPERATIONAL

THERMAL SHOCK

Rapid changes in the temperature of the liquid within the pump can cause thermal shock, which can result in damage or breakage of components and should be avoided.

NEVER APPLY HEAT TO REMOVE IMPELLER Trapped lubricant or vapor could cause an explosion.

HOT (and cold) PARTS

If hot or freezing components or auxiliary heating equipment can present a danger to operators and persons entering the immediate area, action must be taken to avoid accidental contact (such as shielding). If complete protection is not possible, the machine access must be limited to maintenance staff only with clear visual warnings and indicators to those entering



the immediate area. Note: bearing housings must not be insulated and drive motors and bearings may be hot.

If the temperature is greater than 68 °C (175 °F) or below 5 °C (20 °F) in a restricted zone, or exceeds local regulations, action as above shall be taken.

A CAUTION

PREVENT EXCESSIVE EXTERNAL PIPE LOAD

Do not use pump as a support for piping. Do not mount expansion joints, unless allowed by Flowserve in writing, so that their force, due to internal pressure, acts on the pump flange.

CAUTION

ENSURE CORRECT LUBRICATION (See section 5, Commissioning, startup, operation and shutdown.)

CAUTION

NEVER EXCEED THE MAXIMUM DESIGN PRESSURE (MDP) AT THE TEMPERATURE SHOWN ON THE PUMP NAMEPLATE

See section 3 for pressure versus temperature ratings based on the material of construction.

CAUTION NEVER OPERATE THE PUMP WITH THE DISCHARGE VALVE CLOSED

(Unless otherwise instructed at a specific point in the user instructions.)

(See section 5, Commissioning start-up, operation and shutdown.)

CAUTION

NEVER RUN THE PUMP DRY OR WITHOUT PROPER PRIME (Casing Flooded)

CAUTION NEVER OPERATE THE PUMP WITH THE SUCTION VALVE CLOSED

It should be fully opened when the pump is running. CAUTION

NEVER OPERATE THE PUMP AT ZERO FLOW OR FOR EXTENEDED PERIODS BELOW THE MINIMUM CONTINUOUS FLOW

CAUTION THE PUMP SHAFT MUST TURN CLOCKWISE WHEN VIEWED FROM THE MOTOR END

It is absolutely essential that the rotation of the motor be checked before installation of the coupling spacer and starting the pump. Incorrect rotation of the pump for even a short period can unscrew the impeller, which can cause significant damage.

A HAZARDOUS LIQUIDS

When the pump is handling hazardous liquids care must be taken to avoid exposure to the liquid by appropriate pump placement, limiting personnel access and by operator training. If the liquid is flammable and/or explosive, strict safety procedures must be applied.

Gland packing must not be used when pumping hazardous liquids.

1.6.4 Products used in potentially explosive atmospheres



Measures are required to:

- Avoid excess temperature
- Prevent build up of explosive mixtures
- Prevent the generation of sparks
- Prevent leakages
- Maintain the pump to avoid hazard

The following instructions for pumps and pump units when installed in potentially explosive atmospheres must be followed to help ensure explosion protection. Both electrical and non-electrical equipment must meet the requirements of European Directive 94/9/EC.

1.6.4.1 Scope of compliance

Use equipment only in the zone for which it is appropriate. Always check that the driver, drive coupling assembly, seal and pump equipment are suitably rated and/or certified for the classification of the specific atmosphere in which they are to be installed.

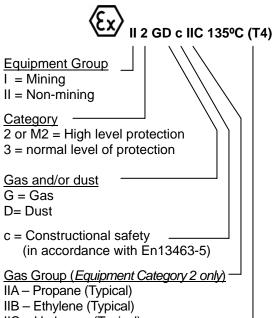
Where Flowserve has supplied only the bare shaft pump, the Ex rating applies only to the pump. The party responsible for assembling the pump set shall select the coupling, driver, seal and any additional equipment, with the necessary CE Certificate/ Declaration of Conformity establishing it is suitable for the area in which it is to be installed.

The output from a variable frequency drive (VFD) can cause additional heating affects in the motor. On pump installations controlled by a VFD, the ATEX Certification for the motor must state that it covers the situation where electrical supply is from the VFD. This particular requirement still applies even if the VFD is in a safe area.



1.6.4.2 Marking

An example of ATEX equipment marking is shown below. The actual classification of the pump will be engraved on the nameplate.



IIC - Hydrogen (Typical)

Maximum surface temperature (Temperature Class) (see section 1.6.4.3)

1.6.4.3 Avoiding excessive surface temperatures ENSURE THE EQUIPMENT TEMPERATURE CLASS IS SUITABLE FOR THE HAZARD ZONE

Pump liquid temperature - Pumps have a temperature class as stated in the ATEX Ex rating on the nameplate. These are based on a maximum ambient temperature of 40°C (104°F); refer to Flowserve for higher ambient temperatures.

The surface temperature on the pump is influenced by the temperature of the liquid handled. The maximum permissible liquid temperature depends on the temperature class and must not exceed the values in the table applicable below. The temperature rise at the seals and bearings and due to the minimum permitted flow rate is taken into account in the temperatures stated.

Maximum permitted liquid temperature for pumps:

Temperature class to EN 13463-1	Maximum surface temperature permitted	Temperature limit of liquid handled (* depending on material and construction variant						
T6	85 °C (185°F)	 – check which is lower) Consult Flowserve 						
T5	100°C (212°F)	Consult Flowserve						
T4	135°C (275°F)	115°C (239°F) *						

The responsibility for compliance with the specified maximum liquid temperature is with the plant operator.

Temperature classification "Tx" is used when the liquid temperature varies and the pump could be installed in different hazardous atmospheres. In this case the user is responsible for ensuring that the pump surface temperature does not exceed that permitted in the particular hazardous atmosphere.

Do not attempt to check the direction of rotation with the coupling element/pins fitted due to the risk of severe contact between rotating and stationary components.

Where there is any risk of the pump being run against a closed valve generating high liquid and casing external surface temperature, it is recommended that users fit an external surface temperature protection device.

Avoid mechanical, hydraulic or electrical overload by using motor overload trips or a power monitor and perform routine vibration monitoring.

In dirty or dusty environments, regular checks must be made and dirt removed from areas around close clearances, bearing housings and motors.

1.6.4.4 Preventing the build up of explosive mixtures



ENSURE PUMP IS PROPERLY FILLED AND VENTED AND DOES NOT RUN DRY

Ensure that the pump and relevant suction and discharge piping is totally filled with liquid at all times during the pumps operation so that an explosive atmosphere is prevented. In addition, it is essential to make sure that seal chambers, auxiliary shaft seal systems and any heating and cooling systems are properly filled.



If the operation of the system can not avoid this condition it is recommended that you fit an appropriate dry run protection device (example: liquid detection or a power monitor).

To avoid potential hazards from fugitive emissions of vapor or gas to atmosphere, the surrounding area must be well ventilated.

1.6.4.5 Preventing sparks $\overline{(c_{1})}$

To prevent a potential hazard from mechanical contact, the coupling guard must be non-sparking for Category 2.

To avoid the potential hazard from random induced current generating a spark, the baseplate must be properly grounded.

Avoid electrostatic charge. Do not rub non-metallic surfaces with a dry cloth; ensure the cloth is damp.

The coupling must be selected to comply with 94/9/EC and correct alignment must be maintained.

Additional requirements for pumps on nonmetallic baseplates - When metallic components are fitted on a non-metallic baseplate they must be individually earthed.

1.6.4.6 Preventing Leakage

Pumps with mechanical seal must only be used to handle liquids for which it has been approved to have the correct corrosion resistance.

Avoid entrapment of liquid in the pump and associated piping due to closing of suction and discharge valves, which could cause dangerous excessive pressures to occur if there is heat input to the liquid. This can occur if the pump is stationary or running.

Bursting of liquid containing parts due to freezing must be avoided by draining or protecting the pump and auxiliary systems.

Where there is the potential hazard of a loss of a seal barrier fluid or external flush, the fluid must be monitored.

If leakage of liquid to atmosphere can result in a hazard, the installation of a liquid detection device is recommended.

1.6.4.7 Maintenance of the centrifugal pump to avoid a hazard

CORRECT MAINTENANCE IS REQUIRED TO AVOID POTENTIAL HAZARDS WHICH GIVE A RISK OF EXPLOSION

The responsibility for compliance with maintenance instructions is with the plant operator.

To avoid potential explosion hazards during maintenance, the tools, cleaning and painting materials used must not give rise to sparking or adversely affect the ambient conditions. Where there is a risk from such tools or materials, maintenance must be conducted in a safe area. It is recommended that a maintenance plan and schedule be implemented. (See section 6, *Maintenance*.)

1.7 Safety labels

1.7.1 Nameplate

For details of nameplate, see Declaration of Conformity and section 3.

1.7.2 Safety labels

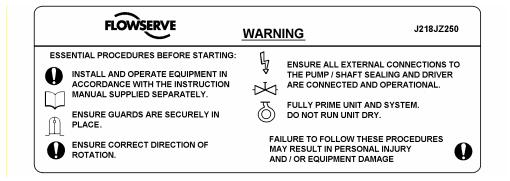


MAX. BOLTING TORQUE = 30 FT. LB.
AUXILIARY CONNECTIONS: DO NOT INSTALL METAL PIPE FITTINGS DIRECTLY INTO PIPE TAPS ON NON-METALLIC PARTS.
PUMP BOLTING:

GLAND NUT TORQUE NOT TO EXCEED 5 FT. LBS. MAIN FLANGE BOLTING NOT TO EXCEED 10 FT.LBS. ALL OTHER BOLTING NOT TO EXCEED 15 FT. LBS.

READ INSTRUCTION BOOK.





ENSURE UNIT ON A FIRM FOUNDATION AND THAT COUPLING FACES ARE IN CORRECT ALIGNMENT PRIOR TO AND AFTER BOLTING BASEPLATE DOWN AND FIXING PIPEWORK. SEE MANUAL FOR TOLERANCES.

S'ASSURER QUE LE GROUPE ELECTROPOMPE EST FERMEMENT INSTALLE SUR SON MASSIF. VERIFIER LE LIGNAGE DE L'ACCOUPLEMENT <u>AVANT ET APRES</u> FIXATION DU SOCLE ET DE LA TUYAUTERIE. VOIR LES TOLERANCES D'ALIGNMENT SUR LA NOTICE PUMP MUSS AUF FESTEM FUNDAMENT STEHEN. KUPPLUNGSHÄLFTEN <u>KORREKT</u> <u>AXIAL AUSRICHTEN</u>. DANN PUMPE AUF GRUNDPLATTE FESTSPANNEN UND ANSSCHLUSSLEITUNGEN BEFESTIGEN. TOLERANZEN S. BEDIEUNGSANLEITUNG.

J218/268

ZORG DAT POMPEENHEID OP EEN STEVIGE ONDERGROND OPGESTELD STAAT EN DAT KOPPELING CORRECT UITGELIJNT IS ZOWEL VOOR-ALS NADAT DE GRONDPLAAT MET BOUTEN IS VASTGEZET EN DE LEIDINGEN GEINSTALLEERD ZIJN. ZIE HANDLEIDING VOOR TOELAABARE SPELINGEN.

CDC: 603 604 610 612 621 623 624

Oil lubricated units only:



DurcoShield[™] (Splash / Shaft Guard)



THIS DEVICE IS NOT A CONTAINMENT SYSTEM NOR A SEAL BACK UP SYSTEM IT IS A LIMITED PROTECTION DEVICE. IT WILL REDUCE BUT NOT ELIMINATE THE PROBABILITY OF INJURY.



1.8 Noise level

When pump noise level exceeds 85dBA attention must be given to prevailing Health and Safety Legislation, to limit the exposure of plant operating personnel to the noise. The usual approach is to control exposure time to the noise or to enclose the machine to reduce emitted sound. You may have already specified a limiting noise level when the equipment was ordered, however if no noise requirements were defined then machines above a certain power level will exceed 85dBA. In such situations consideration must be given to the fitting of an acoustic enclosure to meet local regulations.

Pump noise level is dependent on a number of factors - the type of driver, the operating capacity, piping design and acoustic characteristics of the building.

Typically sound pressure levels measured in dB, and A-weighted values are shown in the table below. The figures are for reference only, they are subject to a +3 dB tolerance, and cannot be guaranteed. The values are based on the noisiest non-geared electric motors that are likely to be encountered. They represent sound pressure levels at 1 m (3.3 ft) from the directly driven pump, for "free field over a reflecting plane". For estimating sound <u>power</u> level (L_{wA} re 1 pW), add 14dBA to the sound pressure value.

If a pump unit only has been purchased, for fitting with your own driver, then the "pump only" noise levels from the table should be combined with the level for the driver obtained from the supplier. If the motor is driven by an inverter, it may show an increase in noise level at some speeds. Consult a Noise Specialist for the combined calculation.

For units driven by equipment other than electric motors or units contained within enclosures, see the accompanying information sheets and manuals.

Typical sound pressure level, dBA (L_{pA}, at 1 m reference 20 μPa)

Motor size and speed		3550	3550 r/min		r/min	1750	r/min	1450 r/min		
		Pump and Pump F motor only		Pump and motor	Pump only	Pump and motor	Pump only	Pump and motor	Pump only	
kW	(hp)	dBA	dBA	dBA	dBA	dBA	dBA	dBA	dBA	
<0.55	(<0.75)	71	66	64	62	64	62	63	62	
0.75	(1)	74	66	67	62	67	62	63	62	
1.1	(1.5)	74	68	67	64	67	64	65	64	
1.5	(2)	77	70	70	66	70	66	66	66	
2.2	(3)	78	72	71	68	71	68	68	68	
3	(4)	81	74	74	70	74	70	70	70	
4	(5)	82	75	75	71	75	71	71	71	
5.5	(7.5)	90	77	83	73	76	73	72	71	
7.5	(10)	90	78	83	74	77	74	73	72	
11	(15)	91	80	84	76	78	76	74	73	
15	(20)	92	83	85	79	80 79	76	75		
18.5	(25)	92	83	85	79	80	79	76	75	
22	(30)	92	83	85	79	81	79	77	75	
30	(40)	100	85	93	81	84	80	80	76	
37	(50)	100	86	93	82	84	80	80	76	
45	(60)	100	87	93	83	84	80	80	76	
55	(75)	102	88	95	84	86	81	82	77	
75	(100)	100	90	95	86	88	81	83	78	
90	(120)	97	90	92	86	90	81	85	78	
110	(150)	100	91	95	87	91	83	86	79	
150	(200)	101	92	96	88	91	85	86	81	
200	(270)	(1)	(1)	(1)	(1)	(1)	(1)	(1)	85	
300	(400)	-	-	-	-	(1)	(1)	(1)	(1)	

(1) Units in this range are generally job specific and noise levels should be calculated based on actual equipment installed.

For 960 rpm reduce 1450 rpm values by 5 dBA.



2 TRANSPORT AND STORAGE

2.1 Consignment receipt and unpacking

Immediately after receipt of the equipment it must be checked against the delivery/shipping documents for its completeness and that there has been no damage in transportation. Any shortage and/or damage must be reported immediately to Flowserve Pump Division and must be received in writing within one month of receipt of the equipment. Later claims cannot be accepted.

Check all crates, boxes or wrappings for any accessories or spare parts that may be packed separately from the equipment or attached to side walls of the box or equipment.

Each product has a unique serial number. Check that this number corresponds with that advised and quote this number in correspondence, as well as when ordering spare parts or further accessories.

2.2 Handling

Boxes, crates, pallets or cartons may be unloaded using fork-lift vehicles or slings depending on their size and construction.

2.3 Lifting

CAUTION Pumps and motors often have integral lifting lugs or eye bolts. These are intended for use in only lifting the individual piece of equipment.

CAUTION

Do not use eye bolts or cast-in lifting lugs to lift pump, motor and baseplate assemblies.

CAUTION To avoid distortion, the pump unit should be lifted as described in this section.

CAUTION

Care must be taken to lift components or assemblies above the center of gravity to prevent the unit from flipping.

2.3.1 Lifting pump components

2.3.1.1 Casing (1100)

Use a choker hitch through the suction hole and around the casing body.

2.3.1.2 Rear cover (1220)

Use a choker hitch slung through the central seal chamber hole to lift large rear covers.

2.3.1.3 Bearing housing (3200)

Group 1:

Insert a sling between the upper and lower support ribs between the housing barrel and the casing attachment flange. Use a choker hitch when slinging. (Make sure there are no sharp edges on the bottom side of the ribs which could cut the sling.)

Group 2 and 3:

Insert either a sling or hook through the lifting lug located on the top of the housing.

2.3.1.4 Power end

Same as bearing housing.

2.3.1.5 Bare pump

Horizontal Pumps: Sling under the casing and around the outboard end of the bearing housing with separate slings. Choker hitches must be used at both attachment points and pulled tight. The sling lengths should be adjusted to balance the load before attaching the lifting hook.

 ${f M}$ A crane must be used for all pump sets in excess of 25 kg (55 lb). Fully trained personnel must carry out lifting in accordance with local regulations. The driver and pump weights are recorded on their respective nameplates.

2.3.2 Lifting pump, motor and baseplate assembly

If the baseplate has lifting holes cut in the sides at the end, (Type A Group 3, Type D, and Type E bases) insert lifting S hooks at the four corners and use slings or chains to connect to the lifting eye. Do not use slings through the lifting holes because of sharp edges. Other styles of baseplates can be lifted by placing slings slightly outboard from the center of mass of the motor and pump. A spreader bar may be required to maintain the sling spacing during lifting.

2.4 Storage

CAUTION

Store the pump in a clean, dry location away from vibration. Leave flange covers in place to keep dirt and other foreign material out of pump casing. Turn the pump shaft at regular intervals to prevent brinelling of the bearings and the seal faces, if fitted, from sticking.



The pump may be stored as above for up to 6 months. Consult Flowserve for preservative actions when a longer storage period is needed.

2.4.1 Short term storage and packaging

Normal packaging is designed to protect the pump and parts during shipment and for dry, indoor storage for up to six months or less. The following is an overview of our normal packaging:

- All loose unmounted items are packaged in a waterproof plastic bag and placed under the coupling guard. Larger items are boxed and metal banded to the baseplate. For pumps not mounted on a baseplate, the bag and/or box is placed inside the shipping container.
- Inner surfaces of the bearing housing, shaft (area through bearing housing) and bearings are coated with Cortec VCI-329 rust inhibitor, or equal. (Note: bearing housings are not filled with oil prior to shipment.)
- Regreasable bearings are packed with grease (EXXON POLYREX EM-FOR HORIZONTAL PUMPS).
- Exposed shafts are taped with Polywrap.
- Flange covers are secured to both the suction and discharge flanges.
- Assemblies ordered with external piping, in some cases components may be disassembled for shipment.

The pump must be stored in a covered, dry location.

2.4.2 Long term storage

Long term storage is defined as more than six months, but less than 12 months. The procedure Flowserve follows for long term storage of pumps is given below. These procedures are in addition to the short term procedure.

- Each assembly is hermetically (heat) sealed from the atmosphere by means of tack wrap sheeting and rubber bushings (mounting holes).
- Desiccant bags are placed inside the tack wrapped packaging.
- A solid wood box is used to cover the assembly.

This packaging will provide protection for up to twelve months from humidity, salt laden air, dust etc. After unpacking, protection will be the responsibility of the user. Addition of oil to the bearing housing will remove the inhibitor. If units are to be idle for extended periods after addition of lubricants, inhibitor oils and greases should be used. Every three months, the pump shaft should be rotated approximately 10 revolutions.

2.5 Recycling and end of product life

At the end of the service life of the product or its parts, the relevant materials and parts should be recycled or disposed of using an environmentally acceptable method and in accordance with local regulations. If the product contains substances that are harmful to the environment, these should be removed and disposed of in accordance with current local regulations. This also includes the liquids and/or gases that may be used in the "seal system" or other utilities.

Make sure that hazardous substances are disposed of safely and that the correct personal protective equipment is used. The safety specifications must be in accordance with the current local regulations at all times.

3 DESCRIPTION

3.1 Configurations

The PolyChem GRP chemical process pumps are end suction, single stage, centrifugal pumps. The GRP family conforms to ASME B73.5M as a nonmetallic wet end, end suction, centerline discharge arrangement. There is also a self-priming option available. These pumps are made of a glassreinforced polymer that is designed to handle a wide range of chemicals. PolyChem GRP pumps may often be used as a cost-effective solution where Stainless Steel, Alloy 20, Monel, Nickel, Hastelloy [™], and even Titanium metal pumps are used.



3.2 Nomenclature

The pump size will be engraved on the nameplate typically as below:

2K 4 X 3G – 13 / 12.5

Frame size: "2K' indicates a medium size pump frame with a Mark3 power end - in this example, a Group 2. 1J or 1K = Group 1 (small frame) 2K = Group 2 (medium frame) 3J = Group 3 (large frame - 2 3/8 inch shaft) 4J = Group 4 (large frame - 2 3/4 inch shaft) Power end: Mark 3A – Standard ANSI 3A - Optional (3 year guarantee) "4" = Nominal suction port size. "3" = Nominal discharge port size. "G" = PolyChem GRP pump line "GS" = Self-primer version Nominal maximum impeller diameter "13" = 13 inch Actual impeller size "12.5" = 12 1/2 in. diameter An example of the nameplate used on the PolyChem

GRP pump is shown below. This nameplate, which is always mounted on the Mark 3 bearing housing, is shown in Figure 3-1

Figure 3-1



3.3 Design of major parts

3.3.1 Pump casing

The pump casing is designed with a horizontal centerline suction inlet and a vertical centerline top discharge which makes it self venting.

Removal of the casing is not required when performing maintenance of the rotating element. The pump is designed with a gasket perpendicular to the shaft allowing the rotating element to be easily removed (back pull out).

3.3.2 Impeller

An open impeller design is the only offering.

3.3.3 Shaft / Sleeve

The pump shafts are sleeved, supported on rolling element bearings, with both threaded and polygon drive ends for the impeller, and a keyed drive end.

3.3.4 Pump bearings and lubrication

Ball bearings are fitted as standard and may be either oil or grease lubricated.

3.3.5 Bearing housing

Options include a large reservoir for oil bath lubrication or the use of zerk fittings for regreasable bearings. A micrometer shaft adjustment allows external setting of the impeller gap.

3.3.6 Seal chamber (cover plate)

The seal chamber has a spigot (rabbet) fit between the pump casing and bearing housing (adapter) for optimum concentricity. The design enables a number of sealing options to be fitted.

3.3.7 Shaft seal

The mechanical seal(s), attached to the pump shaft, seals the pumped liquid from the environment. Gland packing may be fitted as an option.

3.3.8 Driver

The driver is normally an electric motor. Different drive configurations may be fitted such as internal combustion engines, turbines, hydraulic motors etc driving via couplings, belts, gearboxes, drive shafts etc.

3.3.9 Accessories

Accessories may be fitted when specified by the customer.



3.4 Performance and operation limits

This product has been selected to meet the specification of your purchase order see section 1.5.

Typical materials used in the PolyChem GRP include:

<u>Casing, impeller, rear cover, and glands</u> – glass reinforced plastic (GRP) composed of chopped fiberglass strands in a Derakane 470[™] vinyl ester resin. Durcon 730, a glass reinforced thermo-setting epoxy resin, is used for the 1K3x2GS-7.

<u>Shaft sleeves</u> – Ryton® plastic (Polyphenylene sulfide) or high alloy steels are available.

<u>Shafting</u> – 4140 carbon steel as standard with 17-4 PH stainless steel as an option. Superchlor 77 is the standard shaft material for the 1K3x2GS-7 pump.

3.4.1 Pressure-Temperature ratings

Figure 3-2	Bar						
Size	-46 °C	66 °C	121 °C				
1J1.5x1G-6	13.79	13.79	10.34				
1J3x1.5G-6	13.79	13.79	10.34				
1J3x2G-6	13.79	13.79	10.34				
1J1.5x1G-8	13.79	13.79	10.34				
2K3x1.5G-8	13.79	13.79	10.34				
2K3x2G-8	13.79	13.79	10.34				
2K4x3G-8	13.79	13.79	10.34				
2K2x1G-10	17.24	17.24	13.79				
2K3x1.5G-10	6.89	6.89	5.17				
2K4x3G-10	6.89	6.89	5.17				
2K6x4G-10	6.89	6.89	5.17				
2K3x1.5G-13	8.62	8.62	6.89				
2K4x3G-13	8.62	8.62	6.89				
3J8x6G-13	10.34	10.34	8.62				
3J12x10G-15	6.89	6.89	5.17				
4J12x10G-15B	6.89	6.89	5.17				
Size	-29 °C	66 °C	107 °C				
1K3x2GS-7	9.31	9.31	9.31				

Figure 3-3	PSI							
Size	-50 °F	150 °F	250 °F					
1J1.5x1G-6	200	200	150					
1J3x1.5G-6	200	200	150					
1J3x2G-6	200	200	150					
1J1.5x1G-8	200	200	150					
2K3x1.5G-8	200	200	150					
2K3x2G-8	200	200	150					
2K4x3G-8	200	200	150					
2K2x1G-10	250	250	200					
2K3x1.5G-10	100	100	75					
2K4x3G-10	100	100	75					
2K6x4G-10	100	100	75					
2K3x1.5G-13	125	125	100					
2K4x3G-13	125	125	100					
3J8x6G-13	150	150	125					
3J12x10G-15	100	100	75					
4J12x10G-15B	100	100	75					
Size	-20 °F	150 °F	225 °F					
1K3x2GS-7	135	135	135					

The pressure-temperature charts for PolyChem GRP pumps are shown in Figures 3-2 and 3-3. Maximum fluid temperature for Derakane 470[™] material is 121C (250 °F) and for Durcon 730 material is 107C (225 °F).

The following data are typical, and factors such as liquid being pumped, temperature, and seal type may influence them. If required, a definitive statement for your application can be obtained from Flowserve.



3.4.2 Minimum continuous flow

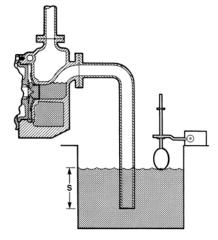
The minimum continuous flow (MCF) is based on a percentage of the best efficiency point (BEP). Figure 3-4 identifies the MCF for all PolyChem GRP pump models.

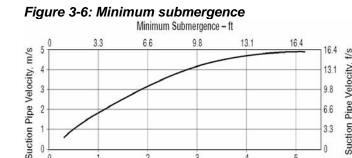
Figure 3-4		MCF	(% of	BEP)
	3600	3000	1800	1200
Size	r/min	r/min	r/min	r/min
1J1.5x1G-6	10	10	10	10
1J3x1.5G-6	10	10	10	10
1J3x2G-6	10	10	10	10
1J3x2GS-7	10	10	10	10
1J1.5x1G-8	10	10	10	10
2K3x1.5G-8	10	10	10	10
2K3x2G-8	10	10	10	10
2K4x3G-8	20	20	20	20
2K2x1G-10	10	10	10	10
2K3x1.5G-10	NA	10	10	10
2K4x3G-10	NA	25	25	25
2K6x4G-10	NA	25	25	25
2K3x1.5G-13	NA	NA	25	25
2K4x3G-13	NA	NA	25	25
3J8x6G-13	NA	NA	25	25
3J12x10G-15	NA	NA	NA	25
4J12x10G-15B	NA	NA	25	25

3.4.3 Minimum suction pipe submergence

The minimum submergence is shown in figure 3-5 and 3-6 for the 1K3x2GS-7 unitized self-priming pump.

Figure 3-5: Minimum submergence





Pipe Velocity,

Suction



3

4

5

2

3.4.4 Suction Pressure Limits

Open style impellers typically create a thrust load towards the suction of the pump. This reduces the axial loading on the bearings so that the suction pressure limit is equal to the pressure-temperature rating.

4 INSTALLATION

0

Equipment operated in hazardous locations must comply with the relevant explosion protection regulations. See section 1.6.4, Products used in potentially explosive atmospheres.

4.1 Location

The pump should be located to allow room for access, ventilation, maintenance, and inspection with ample headroom for lifting and should be as close as practicable to the supply of liquid to be pumped.

Refer to the general arrangement drawing for the pump set.

4.2 Part Assemblies

The supply of motors and baseplates are optional. As a result, it is the responsibility of the installer to ensure that the motor is assembled to the pump and aligned as detailed in section 4.5 and 4.8.

4.3 Foundation

4.3.1 Protection of openings and threads

When the pump is shipped, all threads and all openings are covered. This protection/covering should not be removed until installation. If, for any reason, the pump is removed from service, this protection should be reinstalled.



4.3.2 Rigid baseplates - overview

The function of a baseplate is to provide a rigid foundation under a pump and its driver that maintains alignment between the two. Baseplates may be generally classified into two types:

- Foundation-mounted, grouted design (Figure 4-1)
- Stilt mounted, or free-standing (Figure 4-2)

Figure 4-1



Figure 4-2



Baseplates intended for grouted installation are designed to use the grout as a stiffening member. Stilt mounted baseplates, on the other hand, are designed to provide their own rigidity. Therefore, the designs of the two baseplates are usually different.

Regardless of the type of baseplate used, it must provide certain functions that ensure a reliable installation. Three of these requirements are:

- The baseplate must provide sufficient rigidity to assure the assembly can be transported and installed, given reasonable care in handling, without damage. It must also be rigid enough when properly installed to resist operating loads.
- The baseplate must provide a reasonably flat mounting surface for the pump and driver. Uneven surfaces will result in a soft-foot condition that may make alignment difficult or impossible. Flowserve's experience indicates that a baseplate that has a top surface flatness of 1.25 mm / meter (0.015 inch / foot) across the diagonal corners of the baseplate provides such a mounting surface. Therefore, this is the tolerance to which we supply our standard baseplate. Some users may desire an even flatter surface, which can facilitate installation and alignment. Flowserve will supply flatter

- baseplates upon request at extra cost. For example, mounting surface flatness of 0.17 mm/m (0.002 in./ft) is offered on the Flowserve Type E "Ten Point" baseplate shown in Figure 4-1.
- The baseplate must be designed to allow the user to final field align the pump and driver to within their own particular standards and to compensate for any pump or driver movement that occurred during handling. Normal industry practice is to achieve final alignment by moving the motor to match the pump. Flowserve's practice is to confirm in our shop that the pump assembly can be accurately aligned. Before shipment, the factory verifies that there is enough horizontal movement capability at the motor to obtain a "perfect" final alignment when the installer puts the baseplate assembly into its original, top leveled, unstressed condition.

4.3.3 Stilt and spring mounted baseplates

Flowserve offers stilt and spring mounted baseplates. (See Figure 4-2 for stilt mounted option.) The low vibration levels of PolyChem GRP pumps allow the use of these baseplates - provided they are of a rigid design. The baseplate is set on a flat surface with no tie down bolts or other means of anchoring it to the floor.

General instructions for assembling these baseplates are given below. For dimensional information, please refer to the appropriate Flowserve "Sales Print."

4.3.3.1 Stilt mounted baseplate assembly instructions

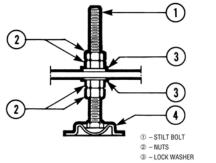
Refer to Figure 4-3

- a) Raise or block up baseplate/pump above the floor to allow for the assembly of the stilts.
- b) Predetermine or measure the approximate desired height for the baseplate above the floor.
- c) Set the bottom nuts (item 2) above the stilt bolt head (item 1) to the desired height.
- d) Assemble lock washer (item 3) down over the stilt bolt.
- e) Assemble the stilt bolt up through hole in the bottom plate and hold in place.
- f) Assemble the lock washer (item 3) and nut (item 2) on the stilt bolt. Tighten the nut down on the lock washer.
- g) After all four stilts have been assembled, position the baseplate in place, over the floor cups (item 4) under each stilt location, and lower the baseplate to the floor.



- Level and make final height adjustments to the suction and discharge pipe by first loosening the top nuts and turning the bottom nuts to raise or lower the baseplate.
- i) Tighten the top and bottom nuts at the lock washer (item 3) first then tighten the other nuts.
- j) It should be noted that the connecting pipelines must be individually supported, and that the stilt mounted baseplate is not intended to support total static pipe load.

Figure 4-3

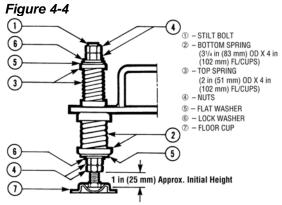


④ – FLOOR CUP

4.3.3.2 Stilt/spring mounted baseplate assembly instructions

Refer to Figure 4-4

- a) Raise or block up baseplate/pump above the floor to allow for the assembly of the stilts.
- b) Set the bottom nuts (item 4) above the stilt bolt head (item 1). This allows for 51 mm (2 in) upward movement for the final height adjustment of the suction/discharge flange.
- c) Assemble the lock washer (item 6) flat washer (item 5) and bottom spring/cup assembly (item 2) down over the stilt bolt (item 1).
- d) Assemble the stilt bolt/bottom spring up through hole in the bottom plate and hold in place.
- e) Assemble top spring/cup assembly (item 3) down over stilt bolt.
- f) Assemble flat washer (item 5), lock washer (item 6) and nuts (item 4) on the stilt bolt.
- g) Tighten down top nuts, compressing the top spring approximately 25 mm (1 in).
- h) After all four stilts have been assembled, position the baseplate in place, over the floor cups (Item 7) under each stilt location, and lower the baseplate down to the floor.
- Level and make final height adjustments to the suction and discharge pipe by first loosening the top nuts, and turning the bottom nuts to raise or lower the baseplate.



- j) To make the stilt bolts more stable, tighten down on the top nuts, compressing the top spring approximately 25 mm (1 in.), and lock the nuts in place.
- k) It should be noted that the connecting pipelines must be individually supported, and that the spring mounted baseplate is not intended to support total static pipe loads.

4.3.3.3 Stilt/spring mounted baseplates - motor alignment

The procedure for motor alignment on stilt or spring mounted baseplates is similar to grouted baseplates. The difference is primarily in the way the baseplate is leveled.

- a) Level the baseplate by using the stilt adjusters. (Shims are not needed as with grouted baseplates.) After the base is level, it is locked in place by locking the stilt adjusters.
- b) Next the initial pump alignment must be checked. The vertical height adjustment provided by the stilts allows the possibility of slightly twisting the baseplate. If there has been no transit damage or twisting of the baseplate during stilt height adjustment, the pump and driver should be within 0.38 mm (0.015 in.) parallel, and 0.0025 mm/mm (0.0025 in./in.) angular alignment. If this is not the case, check to see if the driver mounting fasteners are centered in the driver feet holes.
- c) If the fasteners are not centered there was likely shipping damage. Re-center the fasteners and perform a preliminary alignment to the above tolerances by shimming under the motor for vertical alignment, and by moving the pump for horizontal alignment.



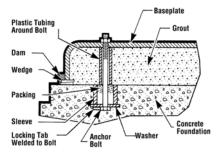
d) If the fasteners are centered, then the baseplate may be twisted. Slightly adjust (one turn of the adjusting nut) the stilts at the driver end of the baseplate and check for alignment to the above tolerances. Repeat as necessary while maintaining a level condition as measured from the pump discharge flange. Lock the stilt adjusters.

The remaining steps are as listed for new grouted baseplates.

4.4 Grouting

 a) The pump foundation should be located as close to the source of the fluid to be pumped as practical. There should be adequate space for workers to install, operate, and maintain the pump. The foundation should be sufficient to absorb any vibration and should provide a rigid support for the pump and motor. Recommended mass of a concrete foundation should be three times that of the pump, motor and base. Refer to Figure 4-5. Note that foundation bolts are imbedded in the concrete inside a sleeve to allow some movement of the bolt.

Figure 4-5



b) Level the pump baseplate assembly. If the baseplate has machined coplanar mounting surfaces, these machined surfaces are to be referenced when leveling the baseplate. This may require that the pump and motor be removed from the baseplate in order to reference the machined faces. If the baseplate is without machined coplanar mounting surfaces, the pump and motor are to be left on the baseplate. The proper surfaces to reference when leveling the pump baseplate assembly are the pump suction and discharge flanges. DO NOT stress the baseplate. Do not bolt the suction or discharge flanges of the pump to the piping until the baseplate foundation is completely installed. If equipped, use leveling jackscrews to level the baseplate. If jackscrews are not provided, shims and wedges should be used (see Figure 4-5).

Check for levelness in both the longitudinal and lateral directions. Shims should be placed at all base anchor bolt locations, and in the middle edge of the base if the base is more than 1.5 m (5 ft) long. Do not rely on the bottom of the baseplate to be flat. Standard baseplate bottoms are not machined, and it is not likely that the field mounting surface is flat.

- c) After leveling the baseplate, tighten the anchor bolts. If shims were used, make sure that the baseplate was shimmed near each anchor bolt before tightening. Failure to do this may result in a twist of the baseplate, which could make it impossible to obtain final alignment. Check the level of the baseplate to make sure that tightening the anchor bolts did not disturb the level of the baseplate. If the anchor bolts did change the level, adjust the jackscrews or shims as needed to level the baseplate. Continue adjusting the jackscrews or shims and tightening the anchor bolts until the baseplate is level.
- Check initial alignment. If the pump and motor d) were removed from the baseplate proceed with step 5 first, then the pump and motor should be reinstalled onto the baseplate using Flowserve's factory preliminary alignment procedure as described in section 4.5, and then continue with the following. As described above, pumps are given a preliminary alignment at the factory. This preliminary alignment is done in a way that ensures that, if the installer duplicates the factory conditions, there will be sufficient clearance between the motor hold down bolts and motor foot holes to move the motor into final alignment. If the pump and motor were properly reinstalled to the baseplate or if they were not removed from the baseplate and there has been no transit damage, and also if the above steps where done properly, the pump and driver should be within 0.38 mm (0.015 in.) FIM (Full Indicator Movement) parallel, and 0.0025 mm/mm (0.0025 in./in.) FIM angular. If this is not the case, first check to see if the driver mounting fasteners are centered in the driver feet holes. If not, re-center the fasteners and perform a preliminary alignment to the above tolerances by shimming under the motor for vertical alignment, and by moving the pump for horizontal alignment.



- e) Grout the baseplate. A non-shrinking grout should be used. Make sure that the grout fills the area under the baseplate. After the grout has cured, check for voids and repair them. Jackscrews, shims and wedges should be removed from under the baseplate at this time. If they were to be left in place, they could rust, swell, and cause distortion in the baseplate.
- Run piping to the suction and discharge of the pump. There should be no piping loads transmitted to the pump after connection is made. Recheck the alignment to verify that there are no significant loads.

4.5 Initial alignment

DANGER Pump and driver must be isolated electrically and the half couplings disconnected.

CAUTION The alignment MUST be checked.

Horizontal initial alignment procedure.

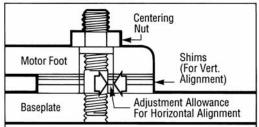
The purpose of factory alignment is to ensure that the user will have full utilization of the clearance in the motor holes for final job-site alignment. To achieve this, the factory alignment procedure specifies that the pump be aligned in the horizontal plane to the motor, with the motor foot bolts centered in the motor holes. This procedure ensures that there is sufficient clearance in the motor holes for the customer to field align the motor to the pump, to zero tolerance. This philosophy requires that the customer be able to place the base in the same condition as the factory. Thus the factory alignment will be done with the base sitting in an unrestrained condition on a flat and level surface. This standard also emphasizes the need to ensure the shaft spacing is adequate to accept the specified coupling spacer.

The factory alignment procedure is summarized below:

- a) The baseplate is placed on a flat and level workbench in a free and unstressed position.
- b) The baseplate is leveled as necessary. Leveling is accomplished by placing shims under the rails of the base at the appropriate anchor bolt hole locations. Levelness is checked in both the longitudinal and lateral directions.
- c) The motor and appropriate motor mounting hardware is placed on the baseplate and the motor is checked for any planar soft-foot condition. If any is present it is eliminated by shimming

d) The motor feet holes are centered on the motor mounting fasteners. This is done by using a centering nut as shown in Figure 4-6.

Figure 4-6



- e) The motor is fastened in place by tightening the nuts on two diagonal motor mounting studs.
- f) The pump is put onto the baseplate and leveled. The foot piece under the bearing housing is adjustable. If an adjustment is necessary, add or remove shims [109A] between the foot piece and the bearing housing.
- g) The spacer coupling gap is verified.
- h) The parallel and angular vertical alignment is made by shimming under the motor.
- The motor feet holes are again centered on the motor mounting studs using the centering nut. At this point the centering nut is removed and replaced with a standard nut. This gives maximum potential mobility for the motor to be horizontally moved during final, field alignment. All four motor feet are tightened down.
- j) The pump and motor shafts are then aligned horizontally, both parallel and angular, by moving the pump to the fixed motor.
- k) The pump feet are tightened down.
- I) Both horizontal and vertical alignment is again final checked as is the coupling spacer gap.

See section 4.8 for Final Shaft Alignment

4.6 Piping

The protective covers are fitted to both the suction and discharge flanges of the casing and must be removed prior to connecting the pump to any pipes.

4.6.1 Suction and discharge piping

All piping must be independently supported, accurately aligned and preferably connected to the pump by a short length of flexible piping. The pump should not have to support the weight of the pipe or compensate for misalignment. It should be possible to install suction and discharge bolts through mating flanges without pulling or prying either of the flanges. All piping must be tight.



Pumps may air-bind if air is allowed to leak into the piping. If the pump flange(s) have tapped holes, select flange fasteners with thread engagement at least equal to the fastener diameter, but that do not bottom out in the tapped holes before the joint is tight.

CAUTION

Never use the pump as a support for piping.

Maximum forces and moments allowed on the pump flanges vary with the pump size and type. To minimize these forces and moments that may, if excessive, cause misalignment, hot bearings, worn couplings, vibration and the possible failure of the pump casing, the following points should be strictly followed:

- Prevent excessive external pipe load •
- Never draw piping into place by applying force to pump flange connections
- Do not mount expansion joints so that their force, due to internal pressure, acts on the pump flange

CAUTION

Ensure piping and fittings are flushed before use.

Ensure piping for hazardous liquids is arranged to allow pump flushing before removal of the pump.

The GRP suction and discharge flanges require full flat face gaskets with a minimum thickness of 3.2 mm (0.125 in.) and a hardness 70 durometer (Shore A).

Check that the gasket material is compatible with the fluid and that the inner diameter of the gasket is centered before assembly.

Use flat washers behind the pump flanges and do not exceed 41 Nm (30 lbf ft) torgue on the flange bolting.

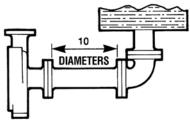
4.6.2 Suction piping

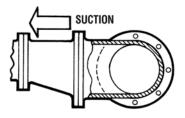
To avoid NPSH and suction problems, suction piping must be at least as large as the pump suction connection. Never use pipe or fittings on the suction that are smaller in diameter than the pump suction size.

Figure 4-7 illustrates the ideal piping configuration with a minimum of 10 pipe diameters between the source and the pump suction. In most cases, horizontal reducers should be eccentric and mounted with the flat side up as shown in Figure 4-8 with a maximum of one pipe size reduction. Never mount eccentric reducers with the flat side down. Horizontally mounted concentric reducers should not

be used if there is any possibility of entrained air in the process fluid. Vertically mounted concentric reducers are acceptable. In applications where the fluid is completely deaerated and free of any vapor or suspended solids, concentric reducers are preferable to eccentric reducers

Figures 4-7 and 4-8





Avoid the use of throttling valves and strainers in the suction line. Start up strainers must be removed shortly before start up. When the pump is installed below the source of supply, a valve should be installed in the suction line to isolate the pump and permit pump inspection and maintenance. However, never place a valve directly on the suction nozzle of the pump.

Refer to the Durco Pump Engineering Manual and the Centrifugal Pump IOM Section of the Hydraulic Institute Standards for additional recommendations on suction piping, section 10. Refer to section 3.4 for performance and operating limits.



4.6.3 Discharge piping

Install a valve in the discharge line. This valve is required for regulating flow and/or to isolate the pump for inspection and maintenance.

CAUTION

When fluid velocity in the pipe is high, for example, 3 m/s (10 ft/sec) or higher, a rapidly closing discharge valve can cause a damaging pressure surge. A dampening arrangement should be provided in the piping.

A non-return valve should be located in the discharge pipework to protect the pump from excessive back pressure and hence reverse rotation when the unit is stopped.

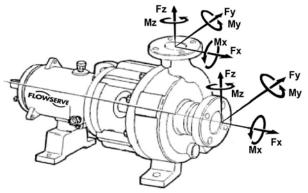
4.6.4 Allowable nozzle loads PolyChem GRP Pumps (ASME B73.5)

Flowserve chemical process pumps meet or exceed the allowable nozzle loads given by ANSI/HI 9.6.2. The following paragraphs describe how to calculate the allowable loads for each pump type and how to determine if the applied loads are acceptable.

The following steps are based upon ANSI/HI 9.6.2. All information necessary to complete the evaluation is given below. For complete details please review the standard.

- a) Find the "Baseplate Correction Factor" in Figure 4-10. The correction factor depends upon how the baseplate is to be installed
- b) The casing material correction factor for the GRP material is 0.9.
- c) Select the lowest correction factor from steps a) and b). Example:-If the pump is mounted on a Type A grouted

Figure 4-9: Coordinate system



- d) baseplate, the correction factor used is 0.9.
 -If the pump is mounted on a Type D stilt mounted baseplate, the correction factor is 0.75.
- e) Locate the pump model being evaluated in Figures 4-12 through 4-15 and multiply each load rating by the lowest correction factor. Record the adjusted loads for each table.
- f) Calculate the applied loads at the casing flanges according to the coordinate system depicted in Figure 4-9. The 12 forces and moments possible are Fxs, Fys, Fzs, Mxs, Mys, Mzs, Fxd, Fyd, Fzd, Mxd, Myd and Mzd. For example, Fxd designates Force in the "x" direction on the discharge flange. Mys designates the Moment about the "y"-axis on the suction flange.
- g) Figure 4-11 gives the acceptance criteria equations. For long coupled pumps, equation sets 1 through 5 must be satisfied.
- h) Equation set 1: Each applied load is divided by the corresponding adjusted Figure 4-12 value. The absolute value of each ratio must be less than or equal to one.
- Equation set 2: The summation of the absolute values of each ratio must be less than or equal to two. The ratios are the applied load divided by the adjusted Figure 4-13 values.
- j) Equation sets 3 and 4: These equations are checking for coupling misalignment due to nozzle loading in each axis. Each applied load is divided by the corresponding adjusted load from Figure 4-14 and 4-15. The result of each equation must be between one and negative one.
- k) Equation set 5: This equation calculates the total shaft movement from the results of equations 3 and 4. The result must be less than or equal to one.

Figure 4-10: Baseplate correction factors

Base Type	Grouted	Bolted	Stilt Mounted
Туре А	1.0	0.7	0.65
Type B - Polybase	1.0	NA	0.95
Туре С	NA	1.0	1.0
Type D	1.0	0.8	0.75
Type E - PIP	1.0	0.95	NA
Polyshield - Baseplate / Foundation	1.0	NA	NA



Figure 4-11: Acceptance criteria equations

Set	Equations	Figure	Remarks
1	$ \left \frac{F_{xs}}{ F_{xs_adj} } \le 1.0, \left \frac{F_{ys}}{ F_{ys_adj} } \le 1.0, \left \frac{F_{zs}}{ F_{zs_adj} } \le 1.0, \left \frac{M_{xs}}{ M_{xs_adj} } \le 1.0, \left \frac{M_{ys}}{ M_{ys_adj} } \le 1.0, \left \frac{M_{zs}}{ M_{zs_adj} } \le 1.0, \left \frac{M_{zs}}{ M_{zd_adj} } \le 1.0, \left \frac{M_{zd}}{ M_{zd_adj} } \le 1.0, \left $	Adjusted 4-12	Maximum individual loading
2	$ \left \frac{F_{XS}}{F_{XS}_adj} \right + \left \frac{F_{yS}}{F_{yS}_adj} \right + \left \frac{F_{zS}}{F_{zS}_adj} \right + \left \frac{M_{xS}}{M_{xS}_adj} \right + \left \frac{M_{yS}}{M_{yS}_adj} \right + \left \frac{M_{zS}}{M_{zS}_adj} \right + \left $	Adjusted 4-13	Nozzle stress, bolt stress, pump slippage
3	$A = \frac{F_{ys}}{F_{ys_adj}} + \frac{M_{xs}}{M_{xs_adj}} + \frac{M_{ys}}{M_{ys_adj}} + \frac{M_{zs}}{M_{zs_adj}} + \frac{M_{zs_adj}}{M_{zs_adj}} + \frac{M_{yd}}{M_{yd_adj}} + \frac{M_{yd}}{M_{zd_adj}} + \frac{M_{zd}}{M_{zd_adj}}$ $-1.0 \le A \le 1.0$	Adjusted 4-14	y-axis movement
4	$B = \frac{F_{xs}}{F_{xs_adj}} + \frac{F_{zs}}{F_{zs_adj}} + \frac{M_{xs}}{M_{xs_adj}} + \frac{M_{ys}}{M_{ys_adj}} + \frac{M_{zs}}{M_{zs_adj}} + \frac{M_{zs_adj}}{M_{zs_adj}} + \frac{F_{zd_adj}}{F_{zd_adj}} + \frac{M_{zd}}{M_{zd_adj}} + \frac{M_{yd}}{M_{yd_adj}} + \frac{M_{zd}}{M_{zd_adj}} + \frac{M_{zd_adj}}{M_{zd_adj}} + $	Adjusted 4-15	z-axis movement
5	$\sqrt{A^2 + B^2} \le 1.0$	-	Combined axis movement

Note: All of the above equations are found by dividing the applied piping loads by the **adjusted** figure values.



	Suction Flange							Discharge Flange					
Pump size	Fo	rces N (I	bf)	Mome	Moments Nm (lbf*ft)			Forces N (lbf)			Moments Nm (lbf*ft)		
	Fxs	Fys	Fzs	Mxs	Mys	Mzs	Fxd	Fyd	Fzd	Mxd	Myd	Mzd	
1J 1.5x1G-6	4 670	3 336	3 336	976	231	231	3 558	6 005	13 344	556	556	556	
	(1 050)	(750)	(750)	(720)	(170)	(170)	(800)	(1350)	(3 000)	(410)	(410)	(410)	
1J 3x1.5G-6	4 670	5 516	5 560	1 220	664	664	3 558	6 005	13 344	678	746	692	
	(1 050)	(1 240)	(1 250)	(900)	(490)	(490)	(800)	(1 350)	(3 000)	(500)	(550)	(510)	
1J 3x2G-6	4 670	4 670	4 670	1 220	298	298	3 558	6 005	13 344	678	1 356	692	
	(1 050)	(1 050)	(1 050)	(900)	(220)	(220)	(800)	(1 350)	(3 000)	(500)	(1 000)	(510)	
1K 3x2GS-7	4 670	4 670	4 670	1 220	298	298	3 558	6 005	13 344	678	1 356	692	
	(1 050)	(1 050)	(1 050)	(900)	(220)	(220)	(800)	(1 350)	(3 000)	(500)	(1 000)	(510)	
1J 1.5x1G-8	4 670	5 382	5 382	976	258	258	3 558	6 005	13 344	488	488	488	
	(1 050)	(1 210)	(1 210)	(720)	(190)	(190)	(800)	(1 350)	(3 000)	(360)	(360)	(360)	
2K 3x1.5G-8	12 010 (2 700)	6 005 (1 350)	6 672 (1 500)	1 763 (1 300)	502 (370)	502 (370)	6 227 (1 400)	6 005 (1 350)	14 456 (3 250)	624 (460)	624 (460)	624 (460)	
2K 3x2G-8	12 010 (2 700)	6 005 (1 350)	6 672 (1 500)	1 763 (1 300)	814 (600)	814 (600)	6 227 (1 400)	6 005 (1 350)	14 456 (3 250)	895 (660)	895 (660)	895 (660)	
2K 4x3G-8	12 010	6 005	6 672	1 763	475	475	6 227	6 005	14 456	1 627	1 980	936	
	(2 700)	(1 350)	(1 500)	(1 300)	(350)	(350)	(1 400)	(1 350)	(3 250)	(1 200)	(1 460)	(690)	
2K 2x1G-10	10 408 (2 340)	4 270 (960)	4 270 (960)	1 722 (1 270)	298 (220)	298 (220)	6 227 (1 400)	6 005 (1 350)	14 456 (3 250)	895 (660)	895 (660)	895 (660)	
2K 3x1.5G-10	12 010	6 005	6 672	1 763	570	570	6 227	6 005	14 456	502	502	502	
	(2 700)	(1 350)	(1 500)	(1 300)	(420)	(420)	(1 400)	(1 350)	(3 250)	(370)	(370)	(370)	
2K 4x3G-10	10 230	6 005	6 672	1 763	420	420	6 227	6 005	14 456	1 627	1 980	936	
	(2 300)	(1 350)	(1 500)	(1 300)	(310)	(310)	(1 400)	(1 350)	(3 250)	(1 200)	(1 460)	(690)	
2K 6x4G-10	12 010 (2 700)	6 005 (1 350)	6 672 (1 500)	1 763 (1 300)	1 492 (1 100)	1 492 (1 100)	6 227 (1 400)	6 005 (1 350)	14 456 (3 250)	1 627 (1 200)	2 034 (1 500)	936 (690)	
2K 3x1.5G-13	12 010	6 005	6 672	1 763	909	909	6 227	6 005	14 456	719	719	719	
	(2 700)	(1 350)	(1 500)	(1 300)	(670)	(670)	(1 400)	(1 350)	(3 250)	(530)	(530)	(530)	
2K 4x3G-13	12 010	6 005	6 672	1 763	542	542	6 227	6 005	14 456	1 627	2 034	936	
	(2 700)	(1 350)	(1 500)	(1 300)	(400)	(400)	(1 400)	(1 350)	(3 250)	(1 200)	(1 500)	(690)	
3J 8x6G-13	15 568	14 145	8 896	2 034	1 587	1 587	6 672	13 344	15 568	1 695	3 851	3 851	
	(3 500)	(3 180)	(2 000)	(1 500)	(1 170)	(1 170)	(1 500)	(3 000)	(3 500)	(1 250)	(2 840)	(2 840)	
3J & 4J 12x10G-15	15 568 (3 500)	14 145 (3 180)	8 896 (2 000)	2 034 (1 500)	1 532 (1 130)	1 532 (1 130)	6 672 (1 500)	13 344 (3 000)	15 568 (3 500)	1 695 (1 250)	3 851 (2 840)	3 851 (2 840)	

Figure 4-12: Maximum individual loading

Figure 4-13: Maximum combined loading

	Suction Flange							Discharge Flange					
Pump size	Fo	Forces N (lbf)			ents Nm	(lbf*ft)	Fo	rces N (I	bf)	Mome	ents Nm	(lbf*ft)	
	Fxs	Fys	Fzs	Mxs	Mys	Mzs	Fxd	Fyd	Fzd	Mxd	Myd	Mzd	
1J 1.5x1G-6	8 985	3 336	3 336	2 481	231	231	8 985	6 005	27 756	556	556	556	
	(2 020)	(750)	(750)	(1 830)	(170)	(170)	(2 020)	(1 350)	(6 240)	(410)	(410)	(410)	
1J 3x1.5G-6	8 985	5 516	9 385	3 105	664	664	8 985	6 005	27 756	746	746	692	
	(2 020)	(1 240)	(2 110)	(2 290)	(490)	(490)	(2 020)	(1 350)	(6 240)	(550)	(550)	(510)	
1J 3x2G-6	8 985	4 670	4 670	3 105	298	298	8 985	6 005	27 756	1 397	1 397	692	
	(2 020)	(1 050)	(1 050)	(2 290)	(220)	(220)	(2 020)	(1 350)	(6 240)	(1 030)	(1 030)	(510)	
1K 3x2GS-7	8 985	4 670	4 670	3 105	298	298	8 985	6 005	27 756	1 397	1 397	692	
	(2 020)	(1 050)	(1 050)	(2 290)	(220)	(220)	(2 020)	(1 350)	(6 240)	(1 030)	(1 030)	(510)	
1J 1.5x1G-8	8 985	5 382	5 382	2 481	258	258	8 985	6 005	27 756	488	488	488	
	(2 020)	(1 210)	(1 210)	(1 830)	(190)	(190)	(2 020)	(1 350)	(6 240)	(360)	(360)	(360)	
2K 3x1.5G-8	12 010	6 005	8 095	5 058	814	502	8 985	6 005	27 756	624	624	624	
	(2 700)	(1 350)	(1 820)	(3 730)	(370)	(370)	(2 020)	(1 350)	(6 240)	(460)	(460)	(460)	
2K 3x2G-8	12 010	6 005	11 076	5 058	814	814	8 763	6 005	27 756	895	895	895	
	(2 700)	(1 350)	(2 490)	(3 730)	(600)	(600)	(1 970)	(1 350)	(6 240)	(660)	(660)	(660)	
2K 4x3G-8	12 010	6 005	8 184	5 058	475	475	8 985	6 005	27 756	1 980	1 980	936	
	(2 700)	(1 350)	(1 840)	(3 730)	(350)	(350)	(2 020)	(1 350)	(6 240)	(1 460)	(1 460)	(690)	
2K 2x1G-10	10 408 (2 340)	4 270 (960)	4 270 (960)	4 936 (3 640)	298 (220)	298 (220)	8 985 (2 020)	6 005 (1 350)	27 756 (6 240)	895 (660)	895 (660)	895 (660)	
2K 3x1.5G-10	12 010	6 005	8 496	5 058	570	570	8 629	6 005	27 756	502	502	502	
	(2 700)	(1 350)	(1 910)	(3 730)	(420)	(420)	(1 940)	(1 350)	(6 240)	(370)	(370)	(370)	
2K 4x3G-10	10 230 (2 300)	6 005 (1 350)	7 295 (1 640)	5 058 (3 730)	420 (310)	420 (310)	8 985 (2 020)	6 005 (1 350)	27 756 (6 240)	1 980 (1 460)	1 980 (1 460)	936 (690)	
2K 6x4G-10	12 010	6 005	27 756	5 058	1 492	1 492	8 985	6 005	27 756	4 204	4 204	936	
	(2 700)	(1 350)	(6 240)	(3 730)	(1 100)	(1 100)	(2 020)	(1 350)	(6 240)	(3 100)	(3 100)	(690)	
2K 3x1.5G-13	12 010	6 005	13 611	5 058	909	909	8 985	6 005	27 756	719	719	719	
	(2 700)	(1 350)	(3 060)	(3 730)	(670)	(670)	(2 020)	(1 350)	(6 240)	(530)	(530)	(530)	
2K 4x3G-13	12 010 (2 700)	6 005 (1 350)	10 631 (2 390)	5 058 (3 730)	542 (400)	542 (400)	8 985 (2 020)	6 005 (1 350)	27 756 (6 240)	2 346 (1 730)	2 346 (1 730)	936 (690)	
3J 8x6G-13	28 289	14 145	22 596	12 163	1 587	1 587	28 289	14 145	59 870	9 194	5 221	3 851	
	(6 360)	(3 180)	(5 080)	(8 970)	(1 170)	(1 170)	(6 360)	(3 180)	(13 460)	(6 780)	(3 850)	(2 840)	
3J & 4J 12x10G-15	28 289	14 145	22 818	12 163	1 532	1 532	28 289	14 145	59 870	12 163	12 285	3 851	
	(6 360)	(3 180)	(5 130)	(8 970)	(1 130)	(1 130)	(6 360)	(3 180)	(13 460)	(8 970)	(9 060)	(2 840)	



		Suction Flange					Discharge Flange					
Forces N (lbf) Mome		oments Nm (lbf*ft)		Fo	Forces N (lbf)		Moments Nm (lbf*ft)		bf*ft)			
Pump size	Fxs	Fys	Fzs	Mxs	Mys	Mzs	Fxd	Fyd	Fzd	Mxd	Myd	Mzd
Group 1		-8 896 (-2 000)		1 220.4 (900)	1 627.2 (1 200)	1 695 (1 250)		6 672 (1 500)		-678 (-500)	2 034 (1 500)	1 695 (1 250)
Group 2		-15 568 (-3 500)		1 762.8 (1 300)	1 762.8 (1 300)	4 068 (3 000)		11 120 (2 500)		-1 627 (-1 200)	2 034 (1 500)	4 068 (3 000)
Group 3		-22 240 (-5 000)		2 034 (1 500)	2 712 (2 000)	5 424 (4 000)		13 344 (3 000)		-1 695 (-1 250)	6 780 (5 000)	5 424 (4 000)

Figure 4-14: Maximum Y-axis loading for shaft deflection

Figure 4-15: Maximum Z-axis loading for shaft deflection

	Suction Flange					Discharge Flange						
Pump size Forces N (lbf) Mo		Mome	Moments Nm (lbf*ft)		Forces N (lbf)		Moments Nm (lbf*ft)					
Fump size	Fxs	Fys	Fzs	Mxs	Mys	Mzs	Fxd	Fyd	Fzd	Mxd	Myd	Mzd
Group 1	4 670 (1 050)		-5 560 (-1 250)	2 034 (1 500)	1 627 (1 200)	-3 390 (-2 500)	3 558 (800)	8 896 (2 000)	-13 344 (-3 000)	-2 034 (-1 500)	1 356 (1 000)	-3 390 (-2 500)
Group 2	15 568 (3 500)		-6 672 (-1 500)	2 034 (1 500)	1 763 (1 300)	-4 746 (-3 500)	6 227 (1 400)	11 120 (2 500)	-14 456 (-3 250)	-2 034 (-1 500)	2 915 (2 150)	-4 746 (-3 500)
Group 3	15 568 (3 500)		-8 896 (-2 000)	2 034 (1 500)	5 560 (4 100)	-5 424 (-4 000)	6 672 (1 500)	17 792 (4 000)	-15 568 (-3 500)	-2 034 (-1 500)	6 780 (5 000)	-5 424 (-4 000)

4.6.5 Pump and shaft alignment check

After connecting the piping, rotate the pump drive shaft clockwise (view from motor end) by hand several complete revolutions to be sure there is no binding and that all parts are free. Recheck shaft alignment (see section 4.5). If piping caused unit to be out of alignment, correct piping to relieve strain on the pump.

4.6.6 Auxiliary Piping

4.6.6.1 Mechanical Seal

When the pump is intended to be equipped with a mechanical seal, it is Flowserve's standard practice to install the mechanical seal in the pump prior to shipment. Specific order requirements may specify that the seal be shipped separately, or none be supplied. It is the pump installer's responsibility to determine if a seal was installed. If a seal was supplied but not installed, the seal and installation instructions will be shipped with the pump.

Failure to ensure that a seal is installed may result in serious leakage of the pumped fluid.

Seal and seal support system must be installed and operational as specified by the seal manufacturer.

The stuffing box/seal chamber/gland may have ports that have been temporarily plugged at the factory to keep out foreign matter. It is the installer's responsibility to determine if these plugs should be removed and external piping connected. Refer to the seal drawings and/or the local Flowserve representative for the proper connections.

When installing piping, do not install metal pipe fittings directly into the non metallic threaded connections on the pump. If metal pipe fittings must be used, then install a non metallic pipe nipple into the connection on the pump and then connect metal pipework to this nipple.

Single seals requiring re-circulation will normally be provided with the auxiliary piping from pump casing already fitted.

Seal housings/covers having an auxiliary quench connection require connection to a suitable source of liquid flow, low pressure steam or static pressure from a header tank. Recommended pressure is 0.35 bar (5 psi) or less. Check *General arrangement drawing*.

Double seals require a barrier liquid between the seals, compatible with the pumped liquid.

With back-to-back double seals, the barrier liquid should be at a minimum pressure of 1 bar above the maximum pressure on the pump side of the inner seal. The barrier liquid pressure must not exceed limitations of the seal on the atmospheric side. For toxic service the barrier liquid supply and discharge must be in a safe area.

Special seals may require modification to auxiliary piping described above. Consult Flowserve if unsure of correct method or arrangement.



For pumping hot liquids, to avoid seal damage, it is recommended that any external flush/cooling supply be continued after stopping the pump.

Tandem seals require a barrier liquid between the seals compatible with the pumped liquid.

4.6.6.2 Packing

When the pump is intended to be equipped with shaft packing, it is not Flowserve's standard practice to install the packing in the stuffing box prior to shipment. The packing is shipped with the pump. It is the pump installer's responsibility to install the packing in the stuffing box.

Failure to ensure that packing is installed may result in serious leakage of the pumped fluid.

4.6.6.3 Piping connection – Seal/packing Support System



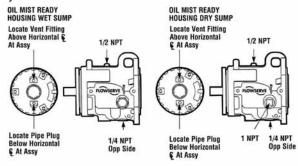
If the pump has a seal support system it is mandatory that this system be fully installed and operational before the pump is started.

<u>Packing lubrication</u> – Water, when compatible with the pumpage, should be introduced into the seal gland at pressure 0.69 to 1.03 bar (10 to 15 psi) above the stuffing box pressure. The gland should be adjusted to give a flow rate of 20 to 30 drops per minute for clean fluid. For abrasive applications, the regulated flow rate should be 0.22 to 0.47 m³/h (1 to 2 US gpm)

Grease lubrication, when compatible with the liquid being pumped, may be used. In non-abrasive applications the liquid being pumped may be sufficient to lubricate the packing without need for external lines.

4.6.6.4 Piping connection - Oil mist lubrication system

The piping connections for an oil mist lubrication system follow:



4.6.6.5 Piping connection – Air Bleed Line

The 1K3x2GS-7 self-priming pump evacuates the air from the suction line when it primes. The length of the line and diameter determine the volume of air and the time required for priming. Flowserve recommends that a small air bleed line be fitted from the discharge piping to the sump if the air is not able to freely vent out the discharge pipe.

4.7 Electrical connections

Anger Electrical connections must be made by a qualified Electrician in accordance with relevant local national and international regulations.

It is important to be aware of the EUROPEAN DIRECTIVE on potentially explosive areas where compliance with IEC60079-14 is an additional requirement for making electrical connections.

Lt is important to be aware of the EUROPEAN DIRECTIVE on electromagnetic compatibility when wiring up and installing equipment on site. Attention must be paid to ensure that the techniques used during wiring/installation do not increase electromagnetic emissions or decrease the electromagnetic immunity of the equipment, wiring or any connected devices. If in any doubt, contact Flowserve for advice.

DANGER The motor must be wired up in accordance with the motor manufacturer's instructions (normally supplied within the terminal box) including any temperature, earth leakage, current and other protective devices as appropriate. The identification nameplate should be checked to ensure the power supply is appropriate.

See section 5.4, *Direction of rotation* before connecting the motor to the electrical supply.

A device to provide emergency stopping must be fitted.

If not supplied pre-wired to the pump unit, the controller/starter electrical details will also be supplied within the controller/starter.



4.8 Final shaft alignment check

- a) Level baseplate if appropriate.
- b) Mount and level pump if appropriate. Level the pump by putting a level on the discharge flange. If not level, adjust the footpiece by adding or deleting shims from between the footpiece and the bearing housing.
- Check initial alignment. If pump and driver have c) been remounted or the specifications given below are not met, perform an initial alignment as described in Section 4.5. This ensures there will be sufficient clearance between the motor hold down bolts and motor foot holes to move the motor into final alignment. The pump and driver should be within 0.38 mm (0.015 in.) FIM (Full Indicator Movement) parallel, and 0.0025 mm/mm (0.0025 in./in.) FIM angular. Stilt mounted baseplates: If initial alignment cannot be achieved with the motor fasteners centered, the baseplate may be twisted. Slightly adjust (one turn of the adjusting nut) the stilts at the driver end of the baseplate and check for alignment to the above tolerances. Repeat as necessary while maintaining a level condition as measured from the pump discharge flange.
- Run piping to the suction and discharge to the pump. There should be no piping loads transmitted to the pump after connection is made. Recheck the alignment to verify that there are no significant changes.
- Perform final alignment. Check for soft-foot e) under the driver. An indicator placed on the coupling, reading in the vertical direction, should not indicate more than 0.05 mm (0.002 in.) movement when any driver fastener is loosened. Align the driver first in the vertical direction by shimming underneath its feet. When satisfactory alignment is obtained the number of shims in the pack should be minimized. It is recommended that no more than five shims be used under any foot. Final horizontal alignment is made by moving the driver. Maximum pump reliability is obtained by having near perfect alignment. Flowserve recommends no more than 0.05 mm (0.002 in.) parallel, and 0.0005 mm/mm (0.0005 in./in.) angular misalignment (see Section 6.8.4.7).



f)

The pump and motor will normally have to be aligned at ambient temperature with an allowance for thermal expansion at operating temperature. (See chart below) In pump installations involving high liquid temperatures, the unit should be run at the actual operating temperature, shut down and the alignment checked immediately. See chart below for recommended offset:

Pumped fluid temperature	Set the driver shaft
Up to 93 °C (200 °F)	Equal to the pump shaft
93 °C to 121 °C (200 °F to 250 °F)	0.13 mm (0.005 in.) below pump shaft

4.9 Protection systems

The following protection systems are recommended particularly if the pump is installed in a potentially explosive area or is handling a hazardous liquid. If in doubt consult Flowserve.

If there is any possibility of the system allowing the pump to run against a closed valve or below minimum continuous safe flow a protection device should be installed to ensure the temperature of the liquid does not rise to an unsafe level.

If there are any circumstances in which the system can allow the pump to run dry, or start up empty, a power monitor should be fitted to stop the pump or prevent it from being started. This is particularly relevant if the pump is handling a flammable liquid.

If leakage of product from the pump or its associated sealing system can cause a hazard it is recommended that an appropriate leakage detection system is installed.

To prevent excessive surface temperatures at bearings it is recommended that temperature or vibration monitoring are carried out.



5 COMMISSIONING, STARTUP, OPERATION AND SHUTDOWN

5.1 Pre-commission procedure

Pre start-up checks

Prior to starting the pump it is essential that the following checks be made. These checks are all described in detail in the Maintenance Section of this manual.

- Pump and motor properly secured to the baseplate
- All fasteners tightened to the correct torque
- Coupling guard in place and not rubbing
- Rotation check, see section 5.4 This is absolutely essential
- Impeller clearance setting
- Shaft seal properly installed
- Seal support system operational
- Bearing lubrication
- Pump instrumentation is operational
- Pump is primed
- Rotation of shaft by hand

As a final step in preparation for operation, it is important to rotate the shaft by hand to be certain that all rotating parts move freely, and that there are no foreign objects in the pump casing.

5.2 Pump lubricants

5.2.1 Oil bath

Oil bath is available on all product lines with the exception of the In-line pump. The standard bearing housing bearings are oil bath lubricated and are not lubricated by Flowserve. Before operating the pump, fill the bearing housing to the center of the oil sight glass with the proper type oil. (See Figure 5-2 for approximate amount of oil required - do not overfill.)

On the Mark 3A design, an optional oil slinger is available. The oil slinger is not necessary; however, if used, it provides an advantage by allowing a larger tolerance in acceptable oil level. Without an oil slinger, the oil level in the bearing housing must be maintained at $\pm 3 \text{ mm} (\pm^{1}/_{8} \text{ in.})$ from the center of the sight glass. The sight glass has a 6 mm (¼ in) hole in the center of its reflector. The bearing housing oil level must be within the circumference of the center hole to ensure adequate lubrication of the bearings.

See Figure 5-3 for recommended lubricants. DO NOT USE DETERGENT OILS. The oil must be free of water, sediment, resin, soaps, acid and fillers of any kind. It should contain rust and oxidation inhibitors. The proper oil viscosity is determined by the bearing housing operating temperature as given in Figure 5-4.

To add oil to the housing, clean and then remove the vent plug [6521] at the top of the bearing housing, pour in oil until it is visually half way up in the sight glass [3856]. Fill the constant level oiler bottle [3855], if used, and return it to its position. The correct oil level is obtained with the constant level oiler in its lowest position, which results in the oil level being at the top of the oil inlet pipe nipple, or half way up in the sight glass window. Oil must be visible in the bottle at all times.

Note that on ANSI 3A[™] power ends there is no constant level oiler. As stated above, proper oil level is the center of the "bull's eye" sight glass [3856] (Figure 5-1).

Figure 5-1



In many pumping applications lubricating oil becomes contaminated before it loses its lubricating qualities or breaks down. For this reason it is recommended that the first oil change take place after approximately 160 hours of operation, at which time, the used oil should be examined carefully for contaminants. During the initial operating period monitor the bearing housing operating temperature. Record the external bearing housing temperature. See Figure 5-6 for maximum acceptable temperatures. The normal oil change interval is based on temperature and is shown in Figure 5-7.

Figure 5-2: Amount of oil required

Size	Volume
Group 1	250 ml (8.5 oz)
Group 2	950 ml (32 oz)
Group 3	1420 ml (48 oz)
Group 4	1420 ml (48 oz)



riguic	Figure 5.3 Recommended on lubricants							
du	Oil	Splash Iu	Ibrication	Oil mist lubrication				
al pur ation	Viscosity mm²/s 40 ºC	32	68	46				
fug	Temp. max. ºC (ºF)	65 (149)	80 (176)	-				
Centrifugal pump lubrication	Designation according to DIN51502 ISO VG	HL/HLP 32	HL/HLP 68	HL/HLP 46				
	BP	BP Energol HL32 BP Energol HLP32	BP Energol HL68 BP Energol HLP68	BP Energol HL46 BP Energol HLP46				
	DEA	Anstron HL32 Anstron HLP32	Anstron HL68 Anstron HLP68	Anstron HL46 Anstron HLP46				
and lubricants	Elf	OLNA 32 HYDRELEF 32 TURBELF 32	TURBELF SA68	TURBELF SA46				
lbr		ELFOLNA DS32	ELFOLNA DS68	ELFOLNA DS46				
nd Ic	Esso	TERESSO 32 NUTO H32	TERESSO 68 NUTO H68	TERESSO 46 NUTO H46				
companies a	Mobil	Mobil DTE oil light Mobil DTE13 MobilDTE24	Mobil DTE oil heavy medium Mobil DTE26	Mobil DTE oil medium Mobil DTE15M Mobil DTE25				
comp	Q8	Q8 Verdi 32 Q8 Haydn 32	Q8 Verdi 68 Q8 Haydn 68	Q8 Verdi 46 Q8 Haydn 46				
lio	Shell	Shell Tellus 32 Shell Tellus 37	Shell Tellus 01 C 68 Shell Tellus 01 68	Shell Tellus 01 C 46 Shell Tellus 01 46				
	Техасо	Rando Oil HD 32 Rando Oil HD-AZ-32	Rando Oil 68 Rando Oil HD C-68	Rando Oil 46 Rando Oil HD B-46				
	Wintershall (BASF Group)	Wiolan HN32 Wiolan HS32	Wiolan HN68 Wiolan HS68	Wiolan HN46 Wiolan HS46				

Figure 5.3 Recommended oil lubricants

Figure 5-4: General lubricant description

Mineral oil	Quality mineral oil with rust and oxidation inhibitors. Mobil DTE Heavy/Medium (or equivalent)
Synthetic	Royal Purple or Conoco SYNCON (or equivalent). Some synthetic lubricants require Viton O-rings.
Grease	EXXON POLYREX EM (or compatible)

Figure 5-5: Oil viscosity grades

Maximum oil temperature	ISO viscosity grade	Minimum viscosity index
Up to 71 °C (160 °F)	46	95
71°-80 °C (160-175 °F)	68	95
80°-94 °C (175-200 °F)	100	95

Figure 5-6: Maximum external housing temperatures

Lubrication	Temperature
Oil bath	82 °C (180 °F)
Oil mist	82 °C (180 °F)
Grease	94 °C (200 °F)
A	

The maximum temperature that the bearing can be exposed to is 105 °C (220 °F).

Figure 5-7: Lubrication intervals*

Lubricant	Under 71 °C (160 °F)	71-80 °C (160-175 °F)	80-94 °C (175-200 °F)
Grease	6 months	3 months	1.5 months
Mineral oil	6 months	3 months	1.5 months
Synthetic oil**	18 months	18 months	18 months

* Assuming good maintenance and operation practices, and no contamination.

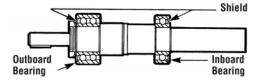
** May be increased to 36 months with ANSI 3A[™] power end.

5.2.2 Grease

5.2.2.1 Regreasable

Single shielded regreasable bearings When the grease lubrication option is specified, single shielded bearings, grease fittings and vent pipe plugs are installed inboard and outboard.

Figure 5-8: Horizontal pump shield orientation

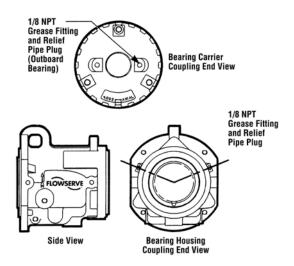




Horizontal pump bearings are packed with Exxon POLYREX EM grease prior to assembly. For relubrication, a grease with the same type base (polyurea) and oil (mineral) should be used. To regrease, remove the pipe plug from both the inboard and outboard bearing location. See Figure 5-9. After relubricating the bearings three times, it is typically recommended that the old grease be cleaned out of the bearing housing.

Make sure to be electrically grounded prior to regreasing in an explosive atmosphere. To regrease bearings under coupling guard, stop pump, lock the motor, remove coupling guard, and then regrease the bearings.

Figure 5-9: Regreasable Configuration



The amount of grease required for horizontal pumps is shown in Figure 5-10.

Housing	Initial Lube	Relubrication	
Group 1 Inboard	Until grease comes out plug	7.5 cm ³ (0.46 in. ³)	
Group 1 Outboard	Until grease comes out plug	14 cm ³ (0.85 in. ³)	
Group 1 Duplex	34 cm ³ (2.1 in ³)	17 cm ³ (1.0 in. ³)	
Group 2 Inboard	Until grease comes out plug	17 cm ³ (1.0 in. ³)	
Group 2 Outboard	Until grease comes out plug	28 cm ³ (1.7 in. ³)	
Group 2 Duplex	68 cm ³ (4.1 in ³)	34 cm ³ (2.1 in. ³)	
Group 3&4 Inboard	Until grease comes out plug	30 cm ³ (1.8 in. ³)	
Group 3&4 Outboard	Until grease comes out plug	54 cm ³ (3.3 in. ³)	
Group 3&4 Duplex	115 cm ³ (7.0 in. ³)	60 cm ³ (3.7 in. ³)	



Do not fill the housing with oil when greased bearings are used. The oil will leach the grease out of the bearings and the life of the bearings may be drastically reduced.

5.2.2.2 Grease for life

Double shielded or double sealed bearings These bearings are packed with grease by the bearing manufacturer and should not be relubricated. The replacement interval for these bearings is greatly affected by their operating temperature and speed. Shielded bearings typically operate cooler.

5.2.3 Oil mist

The inlet port for all horizontal pumps is the plugged ¹/₂ inch NPT located at the top of the bearing housing. A vent fitting has been supplied on the bearing carrier, as well as a plugged ¹/₄ inch NPT bottom drain on the bearing housing. See *Oil mist lubrication system* in Section 4.6.6.4. Do not allow oil level to remain above the center of the bearing housing sight glass window with purge mist (wet sump) systems.

The optional oil slinger must not be used with an oil mist system.

5.3 Impeller clearance

Before carrying out this procedure ensure that the mechanical seal(s) fitted can tolerate a change in their axial setting, otherwise it will be necessary to dismantle the unit and reset the seal axial position after adjusting the impeller clearance.

5.3.1 Final impeller clearance

The open impeller design used by the PolyChem GRP is set off the casing to achieve the final operational gap. The impeller clearance was set at the factory (figure 5-11).

Pump Frame Size	Impeller Gap to Casing	
Group 1 and 2	0.38 mm (0.015 in.)	
3J 8x6G-14	0.51 mm (0.020 in.)	
3J 12x10G-15 & 4J 12x10G-15B	0.63 mm (0.025 in.)	

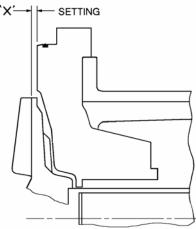


The rotation of bearing carrier from center of one lug on the bearing carrier to center of next lug results in axial shaft movement of 0.1 mm (0.004 in).

5.3.2 Initial impeller setting

Initial impeller clearance is set off the rear cover since the casing is typically left in the piping during servicing of the power end and seal. The initial setting is meant to get the impeller close to the casing so that final adjustment does not upset the mechanical seal setting. The tabulated dimension "X" (see fig. 5-12 & 5-13) can be preset during assembly of the power end prior to installation into the casing.

Figure 5-12 Initial impeller setting



Pump size	Setting distance
1J1k1½ x 1 x 6	3.22 mm (0.127 in.)
1J3 x 1½ x 6	0.91 mm (0.036 in.)
1J3 x 2 x 6K	13.16 mm (0.518 in.)
1J1½ x 1 x 8	0.91 mm (0.036 in.)
2K3 x 1½ x 8	4.16 mm (0.164 in.)
2K3 x 2 x 8	3.17 mm (0.125 in.)
2K4 x 3 x 8	5.51 mm (0.217 in.)
2K2 x 1 x 10	2.36 mm (0.093 in.)
2K3 x 1½ x 10	15.54 mm (0.612 in.)
2K4 x 3 x 10	15.54 mm (0.612 in.)
2K6 x 4 x 10	11.70 mm (0.461 in.)
2K3 x 1½ x 13	0.79 mm (0.031 in.)
2K4 x 3 x 13	0.79 mm (0.031 in.)
3J8 x 6 x 13	1.57 mm (0.062 in.)
3J12 x 10 x 15	17.45 mm (0.687 in)
4J12 x 10 x 15B	17.45 mm (0.687 in)

5.4 Direction of Rotation

5.4.1 Rotation Check

It is absolutely essential that the rotation of the motor be checked before connecting the shaft coupling. Incorrect rotation of the pump, for even a short time, can dislodge and damage the impeller, casing, shaft and shaft seal. All PolyChem GRP pumps turn clockwise as viewed from the motor end. Make sure the motor rotates in the same direction.

If maintenance work has been carried out to the site's electricity supply, the direction of rotation should be re-checked as above in case the supply phasing has been altered.

5.4.2 Coupling Installation

CAUTION The coupling (Figure 5-14) should be installed as advised by the coupling manufacturer. Pumps are shipped without the spacer installed. If the spacer has been installed to facilitate alignment, then it must be removed prior to checking rotation. Remove all protective material from the coupling and shaft before installing the coupling.

Figure 5-14



5.5 Guarding

Power must never be applied to the driver when the coupling guard is not installed.

5.5.1 Clam shell guard - Standard

The standard coupling guard for all PolyChem pumps is the "clam shell" design and is shown in Figure 5-15. It is hinged at the top and it can be removed by loosening one of the foot bolts and sliding the support leg out from under the cap screw (note that the foot is slotted).



The leg can then be rotated upward and half of the guard can be disengaged (unhinged) from the other. Note that only one side of the guard needs to be removed. To reassemble simply reverse the above procedure.

Figure 5-15



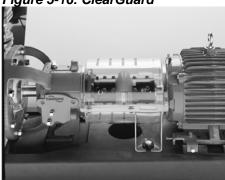
Flowserve coupling guards are safety devices intended to protect workers from inherent dangers of the rotating pump shaft, motor shaft and coupling. It is intended to prevent entry of hands, fingers or other body parts into a point of hazard by reaching through, over, under or around the guard. No standard coupling guard provides complete protection from a disintegrating coupling. Flowserve cannot guarantee their guards will completely contain an exploding coupling.

The coupling guard shown in Figure 5-15 conforms to the USA standard ASME B15.1, "Safety Standard for Mechanical Power Transmission Apparatus." Flowserve manufacturing facilities worldwide conform to local coupling guard regulations.

5.5.2 ClearGuard[™] - Option

Flowserve offers as an option a ClearGuard[™], which allows you to see the condition of the coupling (see Figure 5-16). This guard can be used in palace of the existing clamshell guard described above. The following instructions enable the user to properly fit this guard to the pump and motor.

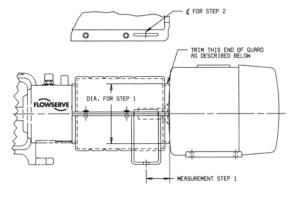
Figure 5-16: ClearGuard™



Trimming and Assembly Instructions

In order to correctly fit the pump/motor configuration, each ClearGuard must be trimmed to a specific length. This trimming is done on the motor end of the guard as described below (see Figure 5-17)

Figure 5-17: ClearGuard™Trimming



5.5.2.1 Trimming instructions

- a) Measure minimum distance from the center of mounting hole in the baseplate to the motor at diameter as shown above.
- b) Locate a reference center of the slot in the coupling guard flange. Transfer measurement from Step 1 to the guard using this reference center.
- c) Trim the motor end of guard according to the above measurement. Trimming is best done with a band saw, but most other types of manual or power saws give acceptable results. Care must be taken to ensure that there is no gap larger than 6 mm (0.24 in.) between the motor and the coupling guard.
- d) Note: If motor diameter is smaller than guard diameter, trim guard so that it extends over the end of the motor as far as possible.
- e) Deburr the trimmed end with a file or a sharp knife. Care must be taken to eliminate all sharp edges.

5.5.2.2 Assembly instructions

- a) Place the bottom and top halves of the ClearGuard around the coupling.
- b) Install the support legs by inserting and then rotating the top flange of the leg through the slot in the shell flange until it comes all the way through and locks the top and bottom together.
- c) Attach the support legs to the baseplate using the fasteners and washers provided.
- d) Install fasteners in the holes provided to secure the guard flanges together.



5.6 Priming and auxiliary supplies

The PolyChem GRP pump will not move liquid unless the pump is primed. A pump is said to be "primed" when the casing and the suction piping are completely filled with liquid. Open discharge valves a slight amount. This will allow any entrapped air to escape and will normally allow the pump to prime, if the suction source is above the pump. When a condition exists where the suction pressure may drop below the pump's capability, it is advisable to add a low-pressure control device to shut the pump down when the pressure drops below a predetermined minimum.

The 1K3x2GS-7 unitized self-priming PolyChem

GRP pump has a different requirement regarding priming. The initial priming liquid must be added to the pump casing until the liquid has reached the bottom of the suction nozzle. Once the initial prime is in place, the pump will automatically replenish itself and be self-priming.

The time required to prime can range from a several seconds to several minutes. If the fluid being pumped is sensitive to temperature change, please contact Flowserve engineering to verify that the temperature increase will not create a dangerous condition inside the pump casing.

5.7 Starting the pump

- a) Open the suction valve to full open position. It is very important to leave the suction valve open while the pump is operating. Any throttling or adjusting of flow must be done through the discharge valve. Partially closing the suction valve can create serious NPSH and pump performance problems.
- b) Never operate pump with both the suction and discharge valves closed. This could cause an explosion.
- c) Ensure the pump is primed. (See section 5.6)
- d) All flush lines must be started and regulated.
- e) Start the driver (typically, the electric motor).
- Slowly open the discharge valve until the desired flow is reached, keeping in mind the minimum continuous flow listed in section 3.4.
- g) It is important that the discharge valve be opened within a short interval after starting the driver. Failure to do this could cause a dangerous build up of heat, and possibly an explosion.

5.8 Running or operation

5.8.1 Minimum continuous flow

Minimum continuous stable flow is the lowest flow at which the pump can operate and still meet the bearing life, shaft deflection and bearing housing vibration limits documented in the latest version of ASME B73.1M. Pumps may be operated at lower flows, but it must be recognized that the pump may exceed one or more of these limits. For example, vibration may exceed the limit set by the ASME standard. The size of the pump, the energy absorbed, and the liquid pumped are some of the considerations in determining the minimum continuous flow (MCF).

The minimum continuous flow (capacity) is established as a percentage of the *best efficiency point* (BEP). See section 3.4.2

5.8.2 Minimum thermal flow

All PolyChem GRP pumps also have a *minimum thermal flow*. This is defined as the minimum flow that will not cause an excessive temperature rise. Minimum thermal flow is application dependent.



Do not operate the pump below minimum thermal flow, as this could cause an excessive temperature rise. Contact a Flowserve Sales Engineer for determination of minimum thermal flow.

Avoid running a centrifugal pump at drastically reduced capacities or with discharge valve closed for extended periods of time. This can cause severe temperature rise and the liquid in the pump may reach its boiling point. If this occurs, the mechanical seal will be exposed to vapor, with no lubrication, and may score or seize to the stationary parts. Continued running under these conditions when the suction valve is also closed can create an explosive condition due to the confined vapor at high pressure and temperature.

Thermostats may be used to safeguard against over heating by shutting down the pump at a predetermined temperature.

Safeguards should also be taken against possible operation with a closed discharge valve, such as installing a bypass back to the suction source. The size of the bypass line and the required bypass flow rate is a function of the input horsepower and the allowable temperature rise.



5.8.3 Reduced head

Note that when discharge head drops, the pump's flow rate usually increases rapidly. Check motor for temperature rise as this may cause overload. If overloading occurs, throttle the discharge.

5.8.4 Surging condition

A rapidly closing discharge valve can cause a damaging pressure surge. A dampening arrangement should be provided in the piping.

5.8.5 Operation in sub-freezing conditions

When using the pump in sub-freezing conditions where the pump is periodically idle, the pump should be properly drained or protected with thermal devices which will keep the liquid in the pump from freezing.

5.8.6 Pumps fitted with a packed gland

If the pump has a packed gland there must be some leakage from the gland. Gland nuts should initially be finger-tight only. Leakage should take place soon after the stuffing box is pressurized.

The gland must be adjusted evenly to give visible leakage and concentric alignment of the gland ring to avoid excess temperature. If no leakage takes place the packing will begin to overheat. If overheating takes place the pump should be stopped and allowed to cool before being re-started. When the pump is re-started, check to ensure leakage is taking place at the packed gland.

If hot liquids are being pumped it may be necessary to slacken the gland nuts to achieve leakage.

The pump should be run for ten minutes with steady leakage and the gland nuts tightened by 10 degrees at a time until leakage is reduced to an acceptable level, normally 30 to 120 drops per minute. Bedding in of the packing may take another 15 minutes.

Care must be taken when adjusting the gland on an operating pump. Safety gloves are essential. Loose clothing must not be worn to avoid being caught up by the pump shaft. Shaft guards must be replaced after the gland adjustment is complete.

Never run gland packing dry, even for a short time.

5.8.7 Bearing monitoring

If the pumps are working in a potentially explosive atmosphere temperature or vibration monitoring at the bearings is recommended If bearing temperatures are to be monitored it is essential that a benchmark temperature is recorded at the commissioning stage and after the bearing temperature has stabilized.

- Record the bearing temperature (t) and the ambient temperature (ta)
- Estimate the likely maximum ambient temperature (tb)
- Set the alarm at (t+tb-ta+5) °C ((t+tb-ta+10) °F) and the trip at 100 °C (212 °F) for oil lubrication and 105 °C (220 °F) for grease lubrication.

It is important, particularly with grease lubrication, to keep a check on bearing temperatures. After start up the temperature rise should be gradual, reaching a maximum after approximately 1.5 to 2 hours. This temperature rise should then remain constant or marginally reduce with time.

Normal vibration levels, alarm and trip

For guidance, pumps generally fall under a classification for rigid support machines within the International rotating machinery standards and the recommended maximum levels below are based on those standards.



Alarm and trip values for installed pumps should be based on the actual measurements taken on the pump in the fully commissioned as new condition. Measuring vibration at regular intervals will then show any deterioration in pump or system operating conditions.

Vibration velocity unfiltered	Power ≤ 15 kW mm/s (in./sec) r.m.s.	Power > 15 kW mm/s (in./sec) r.m.s.
Normal N	≤ 3.0 (0.12)	≤ 4.5 (0.18)
Alarm N x 1.25	≤ 3.8 (0.15)	≤ 5.6 (0.22)
Shutdown trip N x 2.0	≤ 6.0 (0.24)	≤ 9.0 (0.35)



5.9 Stopping and shutdown

Shutdown considerations

When the pump is being shutdown, the procedure should be the reverse of the start-up procedure. First, slowly close the discharge valve, shutdown the driver, and then close the suction valve to isolate the pump if necessary.



Remember that closing the suction valve while the pump is running is a safety hazard and could seriously damage the pump and other equipment.

Switch off flushing liquid supplies at a time appropriate to the process.



For prolonged shut-downs and especially when ambient temperatures are likely to drop below freezing point, the pump and any and flushing arrangements must be drained or otherwise protected.

5.10 Hydraulic, mechanical and electrical duty

5.10.1 Net positive suction head (NPSH)

Net positive suction head - available (NPSH_A) is the measure of the energy in a liquid above the vapor pressure. It is used to determine the likelihood that a fluid will vaporize in the pump. It is critical because a centrifugal pump is designed to pump a liquid, not a vapor. Vaporization in a pump will result in damage to the pump, deterioration of the *Total differential head* (TDH), and possibly a complete stopping of pumping.

Net positive suction head - required (NPSH_R) is the decrease of fluid energy between the inlet of the pump, and the point of lowest pressure in the pump. This decrease occurs because of friction losses and fluid accelerations in the inlet region of the pump and particularly accelerations as the fluid enters the impeller vanes. The value for NPSH_R for the specific pump purchased is given in the pump data sheet, and on the pump performance curve.

For a pump to operate properly the NPSH_A must be greater than the NPSH_R. Good practice dictates that this margin should be at least 1.5 m (5 ft) or 20%, whichever is greater.

CAUTION

Ensuring that $NPSH_A$ is larger than $NPSH_R$ by the suggested margin will greatly enhance pump performance and reliability. It will also reduce the

likelihood of cavitation, which can severely damage the pump.

5.10.2 Specific gravity (SG)

Pump capacity and total head in meters (feet) of liquid do not change with SG, however pressure displayed on a pressure gauge is directly proportional to SG. Power absorbed is also directly proportional to SG. It is therefore important to check that any change in SG will not overload the pump driver or overpressurize the pump.

5.10.3 Viscosity

For a given flow rate the total head reduces with increased viscosity and increases with reduced viscosity. Also for a given flow rate the power absorbed increases with the increased viscosity, and reduces with reduced viscosity. It is important that checks are made with your nearest Flowserve office if changes in viscosity are planned.

5.10.4 Pump speed

Changing the pump speed affects flow, total head, power absorbed, NPSH_R, noise and vibration levels. Flow varies in direct proportion to pump speed. Head varies as speed ratio squared. Power varies as speed ratio cubed. If increasing speed it is important to ensure the maximum pump working pressure is not exceeded, the driver is not overloaded, NPSH_A>NPSH_R and that noise and vibration are within local requirements and regulations.

6 MAINTENANCE

It is the plant operator's responsibility to ensure that all maintenance, inspection and assembly work is carried out by authorized and qualified personnel who have adequately familiarized themselves with the subject matter by studying this manual in detail. (See also section 1.6.2.)

Any work on the machine must be performed when it is at a standstill. It is imperative that the procedure for shutting down the machine is followed, as described in section 5.9.

On completion of work all guards and safety devices must be re-installed and made operative again.



Before restarting the machine, the relevant instructions listed in section 5, *Commissioning, start up, operation and shut down* must be observed.

Oil and grease leaks may make the ground slippery. Machine maintenance must always begin and finish by cleaning the ground and the exterior of the machine.

If platforms, stairs and guard rails are required for maintenance, they must be placed for easy access to areas where maintenance and inspection are to be carried out. The positioning of these accessories must not limit access or hinder the lifting of the part to be serviced.

When air or compressed inert gas is used in the maintenance process, the operator and anyone in the vicinity must be careful and have the appropriate protection.

Do not spray air or compressed inert gas on skin.

Do not direct an air or gas jet towards other people.

Never use air or compressed inert gas to clean clothes.

Before working on the pump, take measures to prevent the pump from being accidentally started. Place a warning sign on the starting device: *"Machine under repair: do not start"*.

With electric drive equipment, lock the main switch open and withdraw any fuses. Put a warning sign on the fuse box or main switch:

"Machine under repair: do not connect".

Never clean equipment with flammable solvents or carbon tetrachloride. Protect yourself against toxic fumes when using cleaning agents.

Refer to the parts list shown in section 8 for item number references used throughout this section.

6.1 Maintenance schedule

It is recommended that a maintenance plan and schedule be implemented, in accordance with these User Instructions, to include the following:

- Any auxiliary systems installed must be monitored, if necessary, to ensure they function correctly.
- b) Gland packing must be adjusted correctly to give visible leakage and concentric alignment of the gland follower to prevent excessive temperature of the packing or follower.

- c) Check for any leaks from gaskets and seals. The correct functioning of the shaft seal must be checked regularly.
- d) Check bearing lubricant level, and the remaining hours before a lubricant change is required.
- e) Check that the duty condition is in the safe operating range for the pump.
- f) Check vibration, noise level and surface temperature at the bearings to confirm satisfactory operation.
- g) Check dirt and dust is removed from areas around close clearances, bearing housings and motors.
- h) Check coupling alignment and re-align if necessary

6.1.1 Preventive maintenance

The following sections of this manual give instructions on how to perform a complete maintenance overhaul. However, it is also important to periodically repeat the *Pre start-up checks* listed in section 5.1. These checks will help extend pump life, as well as the length of time between major overhauls.

6.1.2 Need for maintenance records

A procedure for keeping accurate maintenance records is a critical part of any program to improve pump reliability. There are many variables that can contribute to pump failures. Often long term and repetitive problems can only be solved by analyzing these variables through pump maintenance records.

6.1.3 Cleanliness

One of the major causes of pump failure is the presence of contaminants in the bearing housing. This contamination can be in the form of moisture, dust, dirt and other solid particles such as metal chips. Contamination can also be harmful to the mechanical seal (especially the seal faces), as well as other parts of the pump. For example, dirt in the impeller threads could cause the impeller to not be seated properly against the shaft. This, in turn, could cause a series of other problems. For these reasons, it is very important that proper cleanliness be maintained. Some guidelines are listed below.

After draining the oil from the bearing housing, periodically send it out for analysis. If it is contaminated, determine the cause and correct. The work area should be clean and free from dust, dirt, oil, grease etc. Hands and gloves should be clean. Only clean towels, rags, and tools should be used.



6.2 Spare parts

The decision on what spare parts to stock varies greatly depending on many factors such as the criticality of the application, the time required to buy and receive new spares, the erosive/corrosive nature of the application, and the cost of the spare part. Section 8 identifies all of the components that make up each pump addressed in this manual.

6.2.1 Order of spare parts

Flowserve keeps records of all pumps that have been supplied. Spare parts can be ordered from your local Flowserve Sales Engineer or from a Flowserve Distributor or Representative. When ordering spare parts the following information should be supplied:

- 1) Pump serial number
- 2) Pump size and type
- 3) Part name see section 8
- 4) Part item number see section 8
- 5) Material of construction
- 6) Number of parts required

The pump size and serial number can be found on the name plate located on the bearing housing. See Figure 3-1.

6.3 Recommended spares and consumable items

Recommended spares include: mechanical process fluid seals, bearing housing lip seals, bearings, shafting, impeller, and gaskets.

6.4 Tools required

A typical range of tools that will be required to maintain these pumps is listed below.

6.4.1 Standard hand tools

- Hand wrenches
- Socket wrenches
- Allen wrenches
- Soft mallet
- Screwdrivers

6.4.2 Specialized equipment

- Bearing pullers
- Bearing induction heater
- **Dial indicators**
- Flowserve Mark 3 Tool Kit (see below)

To simplify maintenance, it is recommended that the Flowserve Mark 3 Tool Kit (shown in Figure 6-1) is used. This tool kit includes a handy impeller wrench, which simplifies installation and removal of the impeller.

This tool kit can be ordered from your local Flowserve Sales Engineer or from a Flowserve Distributor or Representative.

Figure 6-1 Flowserve Mark 3 Tool Kit



6.5 Fastener torgues

ltem	Description	Group 1 Non-lubricated	Group 2 Non-lubricated	Group 3 Non-lubricated
N/A	Suction and Discharge flange bolting	41 Nm (30 lbf•ft)	41 Nm (30 lbf•ft)	41 Nm (30 lbf•ft)
[6570.2]	Bearing retainer cap screws	3/16 in 6 Nm (4 lbf•ft)	3/16 in 6 Nm (4 lbf•ft)	5/16 in16 Nm (12 lbf•ft)
[6570.6]	Bearing housing to adapter cap screws	N/A	1/2 in - 54 Nm (40 lbf•ft)	5/8 in - 122 Nm (90 lbf•ft)
[6580.2]	Seal gland nuts	7 Nm (5 lbf•ft)	14 Nm (10 lbf•ft)	14 Nm (10 lbf•ft)
[3712.2]	Impeller nut, polygon drive	27 Nm (20 lbf•ft)	48 Nm (35 lbf•ft)	48 Nm (35 lbf•ft)
[6570.1]	Casing-to-cover bolting	14 Nm (10 lbf•ft)	14 Nm (10 lbf•ft)	14 Nm (10 lbf•ft)
[2912]	Impeller nose cone nut – non-metallic	3 Nm (2 lbf•ft)	3 Nm (2 lbf•ft)	N/A
6570.3]	Bearing carrier set screws	3/8 in. – 16 Nm (12 lbf•ft)	1/2 in 41 Nm (30 lbf•ft)	1/2 in 41 Nm (30 lbf•ft)
6570.5]	Rear foot cap screw	1/2 in 54 Nm (40 lbf•ft)	3/4 in 217 Nm (160 lbf•ft)	1 in 300 Nm (228 lbf•ft)
[6570]	Cap screws – all other with GRP contact	20 Nm (15 lbf•ft)	20 Nm (15 lbf•ft)	20 Nm (15 lbf•ft)

Figure 6-2: Recommended bolt torques - ISO (US)

2.) Gasket joint torque values are for Aflas or 60-70 durometer Viton gaskets. Other gasket materials may require additional torque to seal. Exceeding metal joint torque values is not recommended



6.6 Setting impeller clearance

A new impeller gasket [4590] must be installed whenever the impeller has been removed from the shaft.

Impeller clearance settings may be found in Section 5.3

6.6.1 Initial clearance setting for the PolyChem GRP pumps

Install the impeller [2200] by screwing it onto the shaft (use heavy gloves) until it firmly seats against the shaft shoulder.



The impeller could have sharp edges, which could cause an injury. It is very important to wear heavy gloves.

Tighten the impeller with the impeller wrench from the Flowserve Mark 3 tool kit. To do this, grasp the impeller in both hands and, with the impeller wrench handle to the left (viewed from the impeller end of the shaft) spin the impeller forcefully in a clockwise direction to impact the impeller wrench handle on the work surface to the right (Figure 6-3)

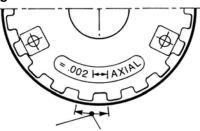
Do not attempt to tighten the impeller on the shaft by hitting the impeller with a hammer or any other object or by inserting a pry bar between the impeller vanes. Serious damage to the impeller may result from such actions.

Figure 6-3



Now set the initial impeller clearance by loosening the set screws [6570.3] and rotating the bearing carrier [3240] to obtain the proper clearance. Turn the bearing carrier counter-clockwise move the impeller towards the rear cover and clockwise to move it away. Use a scale, caliper, or depth gage to measure from the rear cover to the impeller as shown in Figure 5-12. Refer to the charted values in Figure 5-13 for the proper initial impeller clearance as shown in Figure 5-12. Rotating the bearing carrier the width of one of the indicator patterns cast into the bearing carrier moves the impeller axially 0.1 mm (0.004 in.). (Figure 6-5)

Figure 6-5





Rotation Equivalent to 0.1 mm (0.004 in) Axial

Tightening the set screws [6570.3] will cause the impeller to move 0.05 mm (0.002 in.) closer to the rear cover because of the internal looseness in the bearing carrier threads. This must be considered when setting the impeller clearance.

Note: Lastly, uniformly tighten the set screws [6570.3] in incremental steps up to the final torque value to lock the bearing carrier in place.







Example: First, measure the initial distance "X" as shown in figure 5-12. To determine the number of indicator patterns that you will need to rotate the carrier, divide 0.10 (for mm or .004 for inches) into the desired setting. Flowserve suggests that a felt tip pen be used to mark an initial reference point on the bearing housing and the bearing carrier as shown in Figure 6-6. Then make a second mark on the bearing carrier the required number of indicator patterns from the initial reference point. Rotate the bearing carrier until the second mark on the bearing carrier lines up with the initial reference point mark on the bearing housing. Tighten the set screws [6570.3] in incremental steps to lock the bearing carrier in place. The impeller is now set relatively close to its final location. The seal can now be set.

6.6.2 Final clearance setting

Like all front vane semi-open style impellers, the final PGRP open impeller clearance must be set off the casing. The casing must be installed to accurately set the impeller clearance

Attach the power end/rear cover/impeller assembly to the casing. Now set the impeller clearance by loosening the set screws [6570.3] and rotating the bearing carrier [3240] to obtain the proper clearance. Turn the bearing carrier clockwise until the impeller comes into light rubbing contact with the casing. Rotating the shaft at the same time will accurately determine this zero setting. Now, rotate the bearing carrier counter-clockwise to get the proper clearance. Refer to Figure 5-11 for the proper impeller clearance. Rotating the bearing carrier the width of one of the indicator patterns cast into the bearing carrier moves the impeller axially 0.1 mm (0.004 in.). (See Figure 6-5.)

Determine how far to rotate the bearing carrier by dividing the desired impeller clearance by 0.1 mm (0.004 in.) (one indicator pattern). Tightening the set screws [6570.3] will cause the impeller to move 0.05 mm (0.002 in.) away from the casing because of the internal looseness in the bearing carrier threads. This must be considered when setting the impeller clearance. Rotate the bearing carrier counter-clockwise the required amount to get the desired clearance to the casing.

Note:

[6570.3] in incremental steps up to the final torque value to lock the bearing carrier in place.

See section 5.3 for impeller clearance settings.

6.7 Disassembly

6.7.1 Power end removal

 Before performing any maintenance, disconnect the driver from its power supply and lock it off line.

Lock out power to driver to prevent personal injury.

- b) Close the discharge and suction valves, and drain all liquid from the pump.
- c) Close all valves on auxiliary equipment and piping, then disconnect all auxiliary piping.
- d) Decontaminate the pump as necessary.

If Flowserve PolyChem pumps contain dangerous chemicals, it is important to follow plant safety guidelines to avoid personal injury or death.

- e) Remove the coupling guard. (See section 5.5)
- f) Remove the spacer from the coupling.
- g) Remove casing fasteners [6570.1].
- h) Remove the fasteners holding the bearing housing foot to the baseplate.
- i) Move the power end, rear cover, and impeller assembly away from the casing. Discard the casing/cover o-ring [4610.1].

The power end and rear cover assembly is heavy. It is important to follow plant safety guidelines when lifting it.

Figure 6-7

Pump size	Impeller fixing
1J1.5 x 1G - 6	Polygon
1J3 x 1.5G - 6	Threaded
1J3 x 2G - 6K	Polygon
1K3 x 2GS - 7	Threaded
1J1.5 x 1G - 8	Polygon
2K3 x 1.5G - 8	Polygon
2K3 x 2G - 8	Threaded
2K4 x 3G - 8	Polygon
2K2 x 1G - 10	Threaded
2K3 x 1.5G - 10	Polygon
2K4 x 3G - 10	Polygon
2K6 x 4G - 10	Polygon
2K3 x 1.5G - 13	Threaded
2K4 x 3G - 13	Threaded
3J8 x 6G - 13	Threaded
3J12 x 10G – 15	Threaded
4J12 x 10G – 15B	Threaded





6.7.2 Impeller removal

a) Remove the coupling hub from the pump shaft [2100].



Do not apply heat to the impeller. If liquid is entrapped in the hub, an explosion could occur.

- b) For threaded impellers (see Fig. 6-7 and 6-8), use a shaft key [6700] and mount the impeller wrench from the Flowserve Mark 3 Tool Kit (Figure 6-1) to the end of the shaft. With the wrench handle pointing to the left when viewed from the impeller end, grasp the impeller [2200] firmly with both hands (wear heavy gloves). By turning the impeller in the clockwise direction move the wrench handle to the 11:00 o'clock position and then spin the impeller quickly in a counter-clockwise direction so that the wrench makes a sudden impact with a hard surface on the bench. After several sharp raps, the impeller should be free. Unscrew the impeller and remove from the shaft. Discard the impeller-to-sleeve gasket [4590.3].
- c) For polygon drive impellers (see Fig. 6-7), unscrew impeller nose cone nut [2912] and remove impeller nose cone nut gasket [4590.4].
- d) Unscrew impeller stud [2913.1] on Group 1 units, or impeller locknut [3712.2] and washer [6541.6] on Group 2 units.
- e) Rotate the bearing carrier [3240] CCW until the impeller makes contact with the rear cover [1220]. Further rotation will completely loosen the impeller from the shaft [2100].
- f) Remove the impeller-to-sleeve gasket [4590.3].
- g) If a cartridge type mechanical seal [153] is used (Figure 6-9), the spacing clips or tabs should be installed prior to loosening the set screws which attach the seal to the shaft and before removing it form the cover. This will ensure that the proper seal compression is maintained.
- h) Remove the seal or packing gland nuts [6580.2] if so equipped.

Figure 6-8







6.7.3 Removing the rear cover and seal

a) Remove the cover bolts [6570.4] and lockwashers [6541.3] from the bearing housing [3200] (on Group 1 units) or support head [1340] and remove the cover. Sizes 2K3x1.5G-10, 2K4x3G-10 and 2K6x4G-10 do not have bolts so remove the nuts and eccentric washers instead, but there is no need to remove the studs (see Fig. 6-10).



Figure 6-10



- b) Remove the shaft sleeve [2400], gland [4120], and seal [4200].
- c) Remove cover nose gasket [4590.1] (or gland to cover gasket on Group 3) together with the gland [4120] and sleeve-to-shaft O-ring [4610.4] (Groups 1 and 2).
- d) If a component type inside mechanical seal [153] is used, loosen the set screws on the rotating unit and remove it from the shaft (see Figure 6-11). Then pull the gland [4120] and stationary seat off the shaft. Remove the stationary seat from the gland. Discard all Orings and gaskets.

Figure 6-11



- e) If a component type outside mechanical seal is used, remove the gland and the stationary seat. Remove the stationary seat from the gland. Loosen the set screws in the rotating unit and remove it from the shaft. Discard all O-rings and gaskets.
- f) If packing [4130] is used, remove it and the seal cage [4134]. Remove the gland [4120].
- g) The shaft sleeve [2400] can now be removed. Unit now appears as shown in Figure 6-12.

Figure 6-12



6.7.4 Power end disassembly

- a) If the power end is oil lubricated, remove the drain plug [6569] and drain the oil from the bearing housing [3200].
- b) If the pump has lip seals, a deflector [2540] may be present. Slide it off the shaft.
- c) Loosen the three set screws [6570.3] on the bearing carrier [3240]. The bearing carrier must be completely unscrewed from the bearing housing. (Note: Do not pry against the shaft.)

Mark 3A and ANSI 3A design: The face of the bearing carrier has three square lugs that protrude from the surface. The bearing carrier is turned by using an open end wrench on one of the square lugs as shown in Figure 6-13. Because the O-rings [4610.2] will cause some resistance in removing the bearing carrier assembly from the housing, hold the bearing carrier flange firmly and with slight rotation, pull it out of the bearing housing. The bearing carrier assembly with the shaft and bearings should come free. This unit will appear as shown in Figure 6-14. Further disassembly is not required unless the bearings are to be replaced.

Figure 6-13





Figure 6-14



 Remove the snap ring [2530.1] (Figure 6-15) on Group 1 and 2 pumps, or the bearing retainer [2530.2] on Group 3 pumps.

Figure 6-15



Note: Group 1 and 2 pumps equipped with duplex angular contact bearings use a bearing retainer [2530.2] instead of the snap ring. Remove the carrier from the bearing.

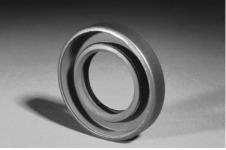
- e) The bearing locknut [3712.1] and lockwasher
 [6541.1] may now be removed from the shaft
 [2100]. Discard the lockwasher.
- f) An arbor or hydraulic press may be used to remove the bearings [3011 and 3013] from the shaft. It is extremely important to apply even pressure to the inner bearing race only. Never apply pressure to the outer race as this exerts excess load on the balls and causes damage.

Applying pressure to the outer race could permanently damage the bearings.

 g) The Mark 3A design has an optional oil slinger [2541] located between the bearings. If present, inspect it for damage or looseness. Remove if it needs to be replaced.

- h) On Group 2 and 3 pumps, the bearing housing [3200] must be separated from the bearing housing adapter [1340]. The adapter O-ring [4610.3] should be discarded.
 Mark 3A and ANSI 3A design: This is accomplished by removing the cap screws [6570.6], which thread into the bearing housing.
- i) If lip seals [4310.1 and 4310.2] (Figure 6-16) are used, they should be removed from the bearing carrier and adapter and discarded.

Figure 6-16



- j) If the bearing isolators are removed from either the bearing carrier or adapter they must not be reused, discard appropriately.
- k) If magnetic seals are used, maintain the seals as specified by the manufacturer.
- *I*) Remove the site gage, oil level tag and oiler, if present.

Mark 3A design: Remove the Trico oiler / site gage [3855] (Figure 6-17) and oil level tag (Figure 6-18) from the bearing housing. *ANSI 3A design*: Remove the site gage [3856] (Figure 5-1) and oil level tag (Figure 6-18) from the bearing housing.

Figure 6-17



Save these parts for reuse.



Figure 6-18 "Oil level must be maintained at center of sight glass"



6.8 Examination of parts

6.8.1 Cleaning/inspection

All parts should now be thoroughly cleaned and inspected. New bearings, O-rings, gaskets, and lip seals should be used. Any parts that show wear or corrosion should be replaced with new genuine Flowserve parts.



It is important that only non-flammable, noncontaminated cleaning fluids are used. These fluids must comply with plant safety and environmental guidelines. Aggressive solvents may damage the GRP material.

6.8.2 Critical measurements and tolerances

To maximize reliability of pumps, it is important that certain parameters and dimensions are measured and maintained within specified tolerances. It is important that all parts be checked. Any parts that do not conform to the specifications should be replaced with new Flowserve parts.

6.8.3 Parameters that should be checked by users

Flowserve recommends that the user check the following measurements and tolerances whenever pump maintenance is performed. Each of these measurements is described in more detail on the following pages.

Figure 6-19

Торіс	ASME B73.5M Std. mm (In.)	Suggested by major seal vendors mm (In.)	Suggested and/ or provided by Flowserve mm (In.)
Shaft Diameter tolerance, under bearings	N.S.		0.005 (0.0002)
Impeller Balance		See note 1	
Bearing housing Diameter (ID) tolerance at bearings	N.S.		0.013 (0.0005)
Power end assembly Shaft runout Shaft sleeve runout Radial deflection - static Shaft endplay	0.05 (0.002) 0.05 (0.002) N.S. N.S.	0.03 (0.001) 0.05 (0.002) 0.076 (0.003) 0.05 (0.002)	0.05 (0.002) 0.05 (0.002) 0.05 (0.002)
Seal chamber Face squareness to shaft Register concentricity	0.08 (0.003)	0.03 (0.001) 0.13 (0.005)	0.08 (0.003) 0.13 (0.005)
Complete pump Shaft movement caused by pipe strain Alignment Vibration at bearing housing	N.S. N.S. See note3	0.05 (0.002)	0.05 (0.002) See note 2 See note 3

N.S. = not specified.

Note 1: The maximum values of acceptable unbalance are: 1500 r/min: 40 g•mm/kg (1800 r/min: 0.021 oz•in./lb.) of mass 2900 r/min: 20 g•mm/kg (3600 r/min: 0.011 oz•in./lb.) of mass The PolyChem GRP impellers conform to the ISO 1940 Grade 6.3 tolerance criteria as molded and are do not require balancing.

Note 2: The ASME B73.5M standard does not specify a recommended level of alignment. Flowserve recommends that the pump and motor shafts be aligned to within 0.05 mm (0.002 in.) parallel FIM (full indicator movement) and 0.0005 mm/mm (0.0005 in./in.) angular FIM. Closer alignment will extend MTBPM. For a detailed discussion of this subject see the *Alignment* section of this manual.

Note 3: The ASME B73.5M, paragraph 5.1.3

6.8.4 Additional parameters checked by Flowserve

The parameters listed below are somewhat more difficult to measure and/or may require specialized equipment. For this reason, they are not typically checked by our customers, although they are monitored by Flowserve during the manufacturing and/or design process.

6.8.4.1 Shaft and sleeve (if fitted)

Replace if grooved, pitted or worn. Prior to mounting bearings or installing the shaft into the bearing housing, check the following parameters.



Diameter / tolerance, under bearings

In order to ensure proper fit between the shaft and bearings, verify that both the inboard (IB) and outboard (OB) shaft diameter is consistently within the minimum/maximum values shown in Figure 6-20. A micrometer should be used to check these outside diameter (OD) dimensions on the shaft.

Figure 6-20

		Group 1	Group 2	Group 3
OB bearing/ shaft	Bearing	30.000/29.990 (1.1811/1.1807)	50.000/49.987 (1.9685/1.9680)	70.000/69.985 (2.7559/2.7553)
mm (in.)	Shaft	30.013/30.003 (1.1816/1.1812)	50.013/50.003 (1.9690/1.9686)	70.015/70.002 (2.7565/2.7560)
	Fit	0.023T/0.003T (0.0009T/0.0001T)	0.026T/0.003T (0.0010T/0.0001T)	0.030T/0.002T (0.0012T/0.0001T)
IB bearing/ shaft	Bearing	35.000/34.989 (1.3780/1.3775)	50.000/49.987 (1.9685/1.9680)	70.000/69.985 (2.7559/2.7553)
mm (in.)	Shaft	35.014/35.004 (1.3785/1.3781)	50.013/50.003 (1.9690/1.9686)	70.015/70.002 (2.7565/2.7560)
	Fit	0.025T/0.004T (0.0010T/0.0001T)	0.026T/0.003T (0.0010T/0.0001T)	0.030T/0.002T (0.0012T/0.0001T)

6.8.4.2 Bearings

It is recommended that bearings not be re-used after removal from the shaft. Prior to mounting bearings, check the following parameters.

Diameter: tolerance, inside diameter

In order to ensure proper fit between bearings and the shaft, verify that the inside diameter (ID) of both the IB and OB bearing are consistently within the minimum/maximum values shown in Figure 6-20. An inside caliper should be used to check these ID diameters on the bearings.

Diameter: tolerance, outside diameter

In order to ensure proper fit between bearings and the bearing housing, verify that the OD on both the IB and OB bearings are consistently within the minimum/maximum values shown in Figure 6-21. A micrometer should be used to check these outside diameter (OD) dimensions on the bearings.

6.8.4.3 Impeller balancing

Shaft whip is deflection where the centerline of the impeller is moving around the true axis of the pump. It is not caused by hydraulic force but rather by an imbalance with the rotating element. Shaft whip is very hard on the mechanical seal because the faces must flex with each revolution in order to maintain contact. To minimize shaft whip it is imperative that the impeller is balanced. All impellers manufactured by Flowserve are balanced after they are trimmed. If for any reason, a customer trims an impeller, it must be re-balanced.

See Note 1 under Figure 6-19 regarding acceptance criteria.

6.8.4.4 Bearing housing and carrier

Prior to installing the shaft into the bearing housing, check the following parameters.

Diameter: tolerance, at bearing surface

In order to ensure proper fit between the bearing housing / carrier and the bearings, verify that the ID of both the IB and OB bearing surfaces are consistently within the minimum/maximum values shown in Figure 6-21. An inside caliper should be used to check these ID dimensions in the bearing housing.

Figure 6-21

		Group 1	Group 2	Group 3
OB	Bearing	71.999/71.986 (2.8346/2.8341)	110.000/109.985 (4.3307/4.3301)	150.000/149.979 (5.9055/5.9047)
bearing/ carrier mm (in.)	Carrier	71.999/72.017 (2.8346/2.8353)	110.007/110.022 (4.3310/4.3316)	150.002/150.030 (5.9056/5.9067)
11111 (111.)	Fit	0.031L/0.000L (0.0012L/0.0000L)	0.037L/0.007L (0.0015/0.0003L)	0.051L/0.002L (0.0020L/0.0001L)
IB booring/	Bearing	71.999/71.986 (2.8346/2.8341)	110.000/109.985 (4.3307/4.3301)	150.000/149.979 (5.9055/5.9047)
bearing/ housing mm (in.)	Housing	71.999/72.017 (2.8346/2.8353)	110.007/110.022 (4.3310/4.3316)	150.007/150.025 (5.9058/5.9065)
	Fit	0.031L/0.000L (0.0012L/0.0000L)	0.037L/0.007L (0.0015L/0.0003L)	0.046L/0.007L (0.0018L/0.0003L)

6.8.4.5 Power end

Assembled bearing housing, carrier, bearings, and shaft.

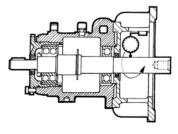
Shaft and shaft sleeve run-out

Shaft run-out is the amount the shaft is "out of true" when rotated in the pump. It is measured by attaching a dial indicator to a stationary part of the pump so that its contact point indicates the radial movement of the shaft surface as the shaft is rotated slowly. If a shaft sleeve is used then shaft sleeve run-out must be checked. It is analogous to shaft run-out. Measurement of shaft run-out/shaft sleeve run-out will disclose any out of roundness of the shaft, any eccentricity between the shaft and the sleeve, any permanent bend in the shaft, and/or any eccentricity in the way the shaft or bearings are mounted in the bearing housing.

Shaft run-out can shorten the life of the bearings and the mechanical seal. The following diagram shows how to measure shaft/shaft sleeve run-out. Note that both ends need to be checked. The runout should be 0.025 mm (0.001 in.) FIM or less.



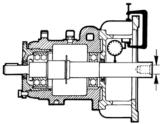
Runout



Radial deflection - static

Radial movement of the shaft can be caused by a loose fit between the shaft and the bearing and/or the bearing and the housing. This movement is measured by attempting to displace the shaft vertically by applying an upward force of approximately 4.5 kg (10 lb.) to the impeller end of the shaft. While applying this force, the movement of an indicator is observed as shown in the following diagram. The movement should be checked at a point as near as possible to the location of the seal faces. A movement of more than 0.05 mm (0.002 in.) is not acceptable.



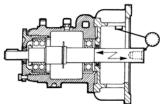


Shaft endplay

The maximum amount of axial shaft movement, or endplay, on a Durco pump should be 0.03 mm (0.001 in.) and is measured as shown below. Observe indicator movement while tapping the shaft from each end in turn with a soft mallet. Shaft endplay can cause several problems. It can cause fretting or wear at the point of contact between the shaft and the secondary sealing element. It can also cause seal overloading or underloading and possibly chipping of the seal faces. It can also cause the faces to

separate if significant axial vibration occurs.

Endplay



6.8.4.6 Seal chamber

Assembled power end and rear cover are checked for face squareness to shaft and register concentricity per Figure 6-19.

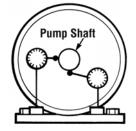
6.8.4.7 Installed pump

Measurements with the complete pump installed.

Shaft movement caused by pipe strain

Pipe strain is any force put on the pump casing by the piping. Pipe strain should be measured as shown below. Install the indicators as shown before attaching the piping to the pump. The suction and discharge flanges should now be bolted to the piping separately while continuously observing the indicators. Indicator movement should not exceed 0.05 mm (0.002 in.).

Pipe Strain Movement



Alignment

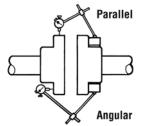
Misalignment of the pump and motor shafts can cause the following problems:

- Failure of the mechanical seal
- Failure of the motor and/or pump bearings
- Failure of the coupling
- Excessive vibration/noise

The schematics below show the technique for a typical rim and face alignment using a dial indicator. It is important that this alignment be done after the flanges are loaded, and at typical operating temperatures. If proper alignment cannot be maintained a C-flange motor adapter and/or stilt/spring mounting should be considered.



Alignment



Many companies today are using laser alignment which is a more sophisticated and accurate technique. This method uses a laser and sensor to measure misalignment. This is fed to a computer with a graphic display that shows the required adjustment side-to-side and shim stock for each of the motor feet to achieve near-perfect alignment.

See section 4.8 for recommended final shaft alignment limits.

Vibration analysis

Vibration analysis is a type of condition monitoring where a pump's vibration "signature" is monitored on a regular, periodic basis. The primary goal of vibration analysis is extension on MTBPM. By using this tool Flowserve can often determine not only the existence of a problem before it becomes serious, but also the root cause and possible solution.

Modern vibration analysis equipment not only detects if a vibration problem exists, but can also suggest the cause of the problem. On a centrifugal pump, these causes can include the following: unbalance, misalignment, defective bearings, resonance, hydraulic forces, cavitation and recirculation. Once identified, the problem can be corrected, leading to increased MTBPM for the pump.

Flowserve does not make vibration analysis equipment, however Flowserve strongly urges customers to work with an equipment supplier or consultant to establish an on-going vibration analysis program. See Note 3 under Figure 6-19 regarding acceptance criteria.

6.9 Assembly of pump and seal

It is important that all pipe threads be sealed properly. PTFE tape provides a very reliable seal over a wide range of fluids, but it has a serious shortcoming if not installed properly. If, during application to the threads, the tape is wrapped over the end of the male thread, strings of the tape will be formed off when threaded into the female fitting. These strings can then tear away and lodge in the piping system. If this occurs in the seal flush system, small orifices can become blocked effectively shutting off flow. For this reason, Flowserve does not recommend the use of PTFE tape as a thread sealant.

Flowserve has investigated and tested alternate sealants and has identified two that provide an effective seal, have the same chemical resistance as the tape, and will not plug flush systems. These are La-co Slic-Tite and Bakerseal. Both products contain finely ground PTFE particles in an oil based carrier. They are supplied in a paste form which is brushed onto the male pipe threads. Flowserve recommends using one of these paste sealants. Full thread length engagement is required for all fasteners.

Note: Refer to Figure 6-2 for recommended bolt torques.

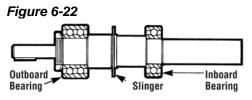
6.9.1 Power end assembly

The Mark 3A design has an optional oil slinger. If the slinger was removed during disassembly, install a new slinger [2541] see Figure 6-22.

6.9.1.1 Bearing installation

Mounting of bearings on shafts must be done in a clean environment. Bearing and power end life can be drastically reduced if even very small foreign particles work their way into the bearings. Wear clean gloves.

Bearings should be removed from their protective packaging only immediately before assembly to limit exposure to possible contamination. After removing the packaging they should only come in contact with clean hands, fixtures, tools and work surfaces.



The chart shown in Figure 6-23 gives the SKF part numbers for bearings in Flowserve Mark 3 pumps. Note that the term "inboard bearing" refers to the bearing nearest to the casing. "Outboard bearing" refers to the bearing nearest to the motor (see Figure 6-22).



Both bearings have a slight interference fit which requires that they be pressed on the shaft with an arbor or hydraulic press. Figure 6-20 identifies the bearing fits. Even force should be applied to only the inner race. Never press on the outer race, as the force will damage the balls and races. An alternate method of installing bearings is to heat the bearings to 93 °C (200 °F) by means of an oven or induction heater. With this approach the bearing must be quickly positioned on the shaft. Never heat the bearings above 110 °C (230 °F). To do so will likely cause the bearing fits to permanently change, leading to early failure.

Group	Type of bearing	Inboard single row, deep groove⁵	Outboard double row, angular contact, deep groove ^{5 & 9}	Optional outboard duplex angular contact⁵
1	Oil bath/mist - open ¹	6207-C3	5306-AC3 or 3306-AC3	7306-BECBY
•	Regreasable - single shielded ²	6207-ZC3	5306-AZC3 or 3306-AZC3	NA ⁶
	Greased for life - double shielded ³	6207-2ZC3	5306-A2ZC3 or 3306-A2ZC3	NA ⁷
	Sealed for life - double sealed ⁴	6207-2RS1C3	5306-A2RSC3 or 3306-A2RS1C3	NA ⁷
2	Oil bath/mist - open ¹	6310-C3	5310-AC3 (AHC3) or 3310-AC3	7310-BECBY
-	Regreasable – single shielded ²	6310-ZC3	5310-AZC3 or 3310-AZC3	NA ⁶
	Greased for life - double shielded ³	6310-2ZC3	5310-A2ZC3 or 3310-A2ZC3	NA ⁷
	Sealed for life - double sealed ⁴	6310-2RS1C3	5310-A2RSC3 or 3310-A2RS1C3	NA ⁷
3	Oil bath/mist - open ¹	6314-C3	5314-AC3 or 3314-AC3	7314-BECBY
3	Regreasable - single shielded ²	6314-ZC3	5314-AZC3 or 3314-AZC3	NA ⁶
	Greased for life - double shielded ³	6314-2ZC3	5314-A2ZC3 or 3314-A2ZC3	NA ⁷
	Sealed for life - double sealed ⁴	6314-2RS1C3	5314-A2RSC3 or 3314-A2RS1C3	NA ⁷

Notes:

1. These bearings are open on both sides. They are lubricated by oil bath or oil mist.

2. These bearings are pre-greased by Flowserve. Replacement bearings will generally not be pre-greased, so grease must be applied by the user. They have a single shield, which is located on the side next to the grease buffer, or reservoir. The bearings draw grease from the reservoir as it is needed. The shield protects the bearing from getting too much grease, which would generate heat. The grease reservoir is initially filled with grease by Flowserve. Lubrication fittings are provided, to allow the customer to periodically replenish the grease, as recommended by the bearing and/or grease manufacturer.

3. These bearings are shielded on both sides. They come pre-greased by the bearing manufacturer. The user does not need to regrease these bearings. The shields do not actually contact the bearing race, so no heat is generated.

- 4. These bearings are sealed on both sides. They come pre-greased by the bearing manufacturer. The user does not need to regrease these bearings. The seals physically contact and rub against the bearing race, which generates heat. These bearings are not recommended at speeds above 1750r/min.
- 5. The codes shown are SKF codes. Inboard and outboard bearings have the C3, greater than "Normal" clearance. These clearances are recommended by SKF to maximize bearing life.
- Regreasable single shielded bearings are not available in the duplex configuration; however, open oil bath-type bearings can be used for the regreasable configuration. These bearings must be pre-greased during assembly. Lubrication fittings are provided, to allow the user to periodically replenish the grease, as recommended by the bearing and/or grease manufacturer.
- Not available.
- 8. All bearing configurations are supplied only with steel cages
- 9. SKF the 5300 and 3300 bearing series are identical and therefore can be used interchangeably.
- a) Install the inboard bearing [3011] on the shaft
 [2100] against the shoulder as shown in Figure
 6-22. If the power end is equipped with single
 shielded regreasable bearings, see Figure 5-8
 for proper orientation of the shields
- b) Install the outboard bearing retaining device onto the shaft.
 Double Row Bearings: Place the snap ring [2530.1] onto the outboard end of the shaft and slide down to the inboard bearing. Note, the proper orientation of the snap ring must be assured in this step. The flat side of the snap

ring must face away from the inboard bearing. Duplex Angular Contact Bearings: Place the bearing retainer [2530.2] onto the outboard end of the shaft and slide down to the inboard bearing. Note, the proper orientation of the bearing retainer must be assured in this step. The small side of the retainer must face away from the inboard bearing.

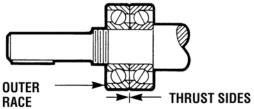


c) Install the outboard bearing.

Double Row Bearings: Install the outboard bearing [3013] firmly against the shoulder as shown in Figure 6-22. If hot bearing mounting techniques are used, steps must be taken to ensure the outboard bearing is firmly positioned against the shaft shoulder. The outboard bearing, while still hot, is to be positioned against the shaft shoulder. Duplex Angular Contact Bearings: Duplex angular contact bearings must be mounted back-to-back with the wider thrust sides of the outer races in contact with each other as shown in Figure 6-24. Only bearings designed for universal mounting should be used. SKF's designation is "BECB". NTN's designation is "G". (Note: A special shaft is required when using duplex angular contact bearings.)

It must be understood that fixtures and equipment used to press the bearing must be designed so no load is ever transmitted through the bearing balls. This would damage the bearing.

Figure 6-24



d) After the bearing has cooled below 38 °C (100 °F) the bearing should be pressed against the shaft shoulder. Figure 6-25 identifies the approximate force needed to seat the bearing against the shaft shoulder. If a press is not available the locknut [3712.1] should be installed immediately after the bearing is placed on the shaft and tightened to ensure the bearing remains in contact with the shaft shoulder. The locknut should then be retightened repeatedly during the time the bearing is cooling. Once cool the locknut should be removed.

Figure 6-25

Pump	Press Force	Locknut Torque
	N (lbf)	N•m (lbf•ft)
Group 1	5,780 (1300)	27 +4/-0 (20 +5/-0)
Group 2	11,100 (2500)	54 +7/-0 (40 +5/-0)
Group 3	20,000 (4500)	95 +7/-0 (70 +5/-0)

e) Install lockwasher [6541.1] and locknut [3712.1]. The locknut should be torqued to the value shown in Figure 6-26. One tang on the lockwasher must be bent into a corresponding groove on the locknut.

6.9.1.2 Bearing housing seals

Lip seals

If lip seals were used (see Figure 6-16), install new lip seals in the bearing carrier [3240] and the housing [3200 - Group 1] or the adapter [1340 - Group 2 and 3]. The lip seals [4310.1 and 4310.2] are double lip style, the cavity between these two lips should be $1/_2$ to $2/_3$ filled with grease. When installing this part, the large metal face on the lip seal must face away from the bearings.

Labyrinth seals

The following are general installation instructions regarding the VBXX Inpro seal. Follow the instructions provided with the seal by the manufacturer.

The elastomer O-ring located on the OD of the seal has been sized to overfill the groove in which it is located. When installing the seal into its corresponding housing, in addition to compressing the o-ring a certain amount of material may shear off. This sheared material should be removed. An arbor press should be used to install the seal.

Install the inboard seal in the bore of the bearing housing (Group 1) or adapter (Group 2 and Group 3) with the single expulsion port positioned at the 6 o'clock position.

Install the outboard seal in the bore of the bearing carrier. There are no orientation issues since this is a multiport design seal.

Magnetic seals

Follow the installation instructions provided by the manufacturer.

6.9.1.3 Bearing carrier/power end assembly

- a) Install new O-rings [4610.2] onto the bearing carrier. Slide the bearing carrier [3240] over the outboard bearing [3013].
- b) Install the outboard bearing retaining device. Double Row Bearings on Group 1 and 2 pumps: Slide the snap ring [2530.1] in place with its flat side against the outboard bearing and snap it into its groove in the bearing carrier. Duplex Angular Contact Bearings on Group 1 and 2 pumps; All Bearings on Group 3 pumps:



Slide the bearing retainer [2530.2] against the outboard bearing and install and tighten the socket head capscrews [6570.2]. See Figure 6-2 for correct torque values.

CAUTION Never compress the snap ring unless it is positioned around the shaft and between the bearings. In this configuration, it is contained therefore if it should slip off the compression tool it is unlikely to cause serious injury.

- c) The shaft, bearings, and bearing carrier assembly (Figure 6-14) can now be installed into the bearing housing [3200]. The bearing carrier [3240] should be lubricated with oil on the O-rings and threads before installing the assembly into the bearing housing. Thread the bearing carrier into the bearing housing by turning it clockwise to engage the threads. Thread the carrier flange is approximately 3mm (¹/₈in) from the housing. Install the set screws [6570.3] loosely.
- Reinstall any tags, plugs, site gages and oiler. Mark 3A design: Install the following items onto the bearing housing; oil level tag (Figure 6-18) and combination Trico oiler / site gage [3855], vent / breather [6521] and drain plug [6569]. ANSI 3A design: Install the following items onto the bearing housing; oil level tag (Figure 6-18) and site gage [3855], plug [6521] and magnetic drain plug [6559].
- e) On Group 2 and 3 pumps, assemble the bearing housing adapter [1340] to the bearing housing [3200]. Be sure to install a new O-ring [4610.3]. Mark 3A and ANSI 3A design: Thread the capscrews [6570.6] through the adapter and into the tapped holes in the bearing housing.
- f) If the power end used lip seals, install the flinger (deflector) [2540] onto the shaft [2100].
- g) Slide the sleeve [2400] onto the shaft ensuring that the flinger o-ring and flinger slip under the end of the sleeve.

6.9.2 Seal and rear cover assembly

- a) With an external seal slide the rotating part of the seal over the sleeve but do not tighten the setscrews at this time.
- b) Position the seat to gland gasket [4590.2] and seal seat into the gland [4120] and slide this assembly over the sleeve.
- c) With a cartridge seal, slide the seal over the sleeve, but do not tighten the setscrews at this time.

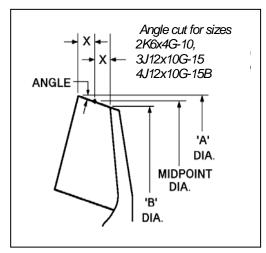
- d) For non-cartridge internal seals, install the stationary seal face and its gasket or O-ring into the gland.
- e) Place the cover nose gasket into the gland (or the cover to gland gasket on Groups 3 and 4) and slide them all over the sleeve.
- f) With an internal seal, position the rotating portion of the seal on the sleeve as shown on the seal drawing provided, or as marked on the sleeve during disassembly. It may be necessary to assemble the pump to the impeller clearance setting stage to properly locate the shaft (if the rotor has been moved). Mark the end of the box on the shaft and then disassemble the pump back to this stage. This is because seal setting is measured from the end of the box.
- g) If they were removed, assemble the gland studs [6572] into the cover [1220], replace the box extension onto the cover and slide the gland over the sleeve.
- h) Assemble the cover onto the bearing housing
 [3200] on Group 1 or support head [1340] using bolts [6570.4] and lockwashers [6541.3] and torque up to 20 Nm (15 lbf·ft). For 2K3x1.5G-10, 2K4x3G-10 and 2K6x4G-10 units use eccentric washers and nuts instead.

6.9.3 Impeller assembly

If a new impeller of maximum diameter has been acquired and needs reducing, or if the existing impeller diameter needs reducing, they must both be machined down to the correct size. It is preferred to send the impeller to your Flowserve representative for machining, but when this is not possible, the following procedure can be used:

- a) Obtain the correct machining mandrel from your Flowserve representative or use the pump shaft and impeller bolting.
- b) Carefully mount the mandrel or shaft in a lathe suitable for machining GRP.
- c) Mount the impeller and, using a dial indicator, verify the outer diameter run-out and impeller face run-out (on the vanes at the outer diameter) are each less than 0.13 mm (0.005 in.) TIR.
- d) Prepare to machine. All impellers are machined straight across, parallel to the shaft except sizes 2K6x4G-10, 3J12x10G-15 and 4J12x10G-15B which have angled cuts. The 2K6x4G-10 vanes are machined at an angle of 15 degrees to the shaft axis whilst the 3J12x10G-15 and 4J12x10G-15B vanes are machined at an angle of 10 degrees to the shaft axis with the larger diameter at the open vane face and the smaller diameter at the back impeller shroud. The listed impeller diameter is the mid-point of the vane. Refer to the sketch for these details:





Midpoint (listed) diameter = $\frac{A + B}{2}$

Angle = 15 degrees (2K6x4G-10) or 10 degrees (3J12x10G-15 and 4J12x10G-15B)

Depth of cut, roughing	5.10 mm (0.200 in.)
Feed rate per revolution	0.38 mm (0.015 in.)
Depth of cut, finishing	0.51 mm (0.020 in.)
Feed rate per revolution	0.08 mm (0.003 in.)
Surface speed per minute	91 to 213 m (300 to 700 ft)

- e) Machining the GRP material produces dust that can be irritating to the operator, but is not hazardous. Dust vacuum systems, skin protection and a dust mask are recommended. A typical machining setup would be as shown below:
- f) Start machining across the outer diameter. Machine from both sides to the middle. Continue with additional cuts until the required impeller diameter is achieved.
- g) The finished impeller can then be removed from the lathe and installed in the pump. No mechanical balancing or resin coating of the vane tips is required.

6.9.3.1 Polygon impeller drive units

- a) Position the impeller to sleeve gasket [4590.3] into the groove on the impeller and push impeller, hand tight, onto the shaft. The impeller is a slight interference fit with the shaft and its face should extend 0.38 mm to 0.89 mm (0.015 in. to 0.035 in.) from the end of the shaft.
- b) Seat the impeller by fitting the impeller stud [2913.1] on Group 1 and torque up to 27 Nm (20 lbf-ft) or on Group 2 fit the washer [6541.6] and locknut [3712.2] and torque up to 48 Nm (35 lbf-ft).

This will push the impeller face down until it lines up with the end of the shaft.

c) Install the impeller nose cone nut gasket [4590.4] on the impeller, fit the impeller nose cone [2912] and tighten hand tight 3 Nm (2 lbf-ft) as this nut does not hold the impeller in place but merely seals the shaft from the fluid.

6.9.3.2 Threaded impeller drive units

- a) Position the impeller to sleeve gasket [4590.3] into the groove on the sleeve or impeller.
- b) Lubricate the impeller threads and pilot fit with light oil having a light graphite suspension.
- c) Locate the impeller on the shaft and thread on.
- d) The impeller clearance should now be pre-set to the tabulated dimensions in section 6.6.

6.9.4 Gland fastening to the cover

- a) For mechanical seals, assemble the gland [4120] onto the gland studs [6572], fit the gland backing plate (if supplied), then fit the gland washers [6541.5] and nuts [6580.2] and torque up evenly to 7 Nm (5 lbf·ft) on Group 1 units and 14 Nm (10 lbf·ft) on all other sizes.
- b) For external seals, position the seal rotating assembly against the seal stationary face, compress the springs as specified on the seal drawing and tighten the seal setscrews evenly.
- c) For cartridge seals, tighten the setscrews evenly and remove the gland centering tabs, but retain for future maintenance.
- d) For packing, install 4 packing rings [4130], then the seal cage [4134] and then 2 more rings of packing.
 Note:
- e) Pump size 4J12x10G-15B only has 5 rings of packing followed by the seal cage and then 2 more rings of packing.)

6.9.5 Final back pullout assembly steps

- a) Refit the constant level oiler, if supplied.
- b) Fit the main casing O-ring [4610.1] onto the cover [1200].
- c) The complete back pullout assembly can now be installed into the casing. Fit the casing bolts [6570.1] or use the studs [6572] (on some pumps) together with washers [6541.4], lockwashers [6541.2] and nuts [6580.3] and torque up evenly to 14 Nm (10 lbf-ft).
- d) Finally, adjust the impeller running clearance as section 6.6.



7 Faults; Causes and Remedies

TROUBLESHOOTING

The following is a guide to troubleshooting problems with Flowserve Mark 3 pumps. Common problems are analyzed and solutions offered. Obviously, it is impossible to cover every possible scenario. If a problem exists that is not covered by one of the examples, then refer to one of the books listed in the Sources of additional information section or contact a Flowserve Sales Engineer or Distributor/Representative for assistance.

FAULT SYMPTOM

D	Rump not reaching design flow rate										
гu	Pump not reaching design flow rate										
Ŷ	Pump not reaching design head (TDH)										
	₽			discharge or flow with pump running							
		₽	Pu	Pump operates for short period, then loses prime							
			₩	E	xce	ssiv	veı	nois	se fi	rom wet end	
				₽	E	хсе	ssi	veı	nois	se from power end	
					₽						
						₽					
							1	<u> </u>			
							ľ	₽			
								ľ	î		1
									ř	PROBABLE CAUSES	POSSIBLE REMEDIES
•	•		•	•						Insufficient NPSH. (Noise may not be present.)	Recalculate NPSH available. It must be greater than the NPSH required by pump at desired flow. If not, redesign suction piping, holding number of elbows and number of planes to a minimum to avoid adverse flow rotation as it approaches the impeller.
•	•	•								System head greater than anticipated.	Reduce system head by increasing pipe size and/or reducing number of fittings. Increase impeller diameter. (NOTE: Increasing impeller diameter may require use of a larger motor.)
•	•		•							Entrained air. Air leak from atmosphere on suction side.	 Check suction line gaskets and threads for tightness. If vortex formation is observed in suction tank, install vortex breaker. Check for minimum submergence
•	•									Entrained gas from process.	Process generated gases may require larger pumps.
•	•									Speed too low.	Check motor speed against design speed.
•	•	•								Direction of rotation wrong.	After confirming wrong rotation, reverse any two of three leads on a three phase motor. The pump should be disassembled and inspected before it is restarted.
•	•									Impeller too small.	Replace with proper diameter impeller. (NOTE: Increasing impeller diameter may require use of a larger motor.)
•	•									Impeller clearance too large.	Reset impeller clearance.
•	•	•								Plugged impeller, suction line or casing which may be due to a product or large solids.	 Reduce length of fiber when possible. Reduce solids in the process fluid when possible. Consider larger pump.
•	•									Wet end parts (casing cover, impeller) worn, corroded or missing.	Replace part or parts.
	•	•								Not properly primed.	Repeat priming operation, recheck instructions. If pump has run dry, disassemble and inspect the pump before operation.
				•						Impeller rubbing.	 Check and reset impeller clearance. Check outboard bearing assembly for axial end play.



FAULT SYMPTOM

<u> </u>	Pump not reaching design flow rate											
¶ U	Pump not reaching design head (TDH)											
Ŷ	1, î		No discharge or flow with pump running									
	Ŷ											
		1 ↑		<u> </u>					short period, then loses prime			
			₩						e from wet end			
				₩	E	xce	ssiv	/e r	noise from power end			
					₽							
						₩						
							₽					
								₽				
									PROBABLE CAUSES	POSSIBLE REMEDIES		
	•	•							Damaged pump shaft, impeller.	Replace damaged parts.		
				•					Abnormal fluid rotation due to complex suction piping.	Redesign suction piping, holding the number of elbows and planes to a minimum to avoid adverse fluid rotation as it approaches the impeller.		
					•				Bearing contamination appearing on the raceways as scoring, pitting, scratching or rusting caused by adverse environment and entrance of abrasive contaminants from atmosphere.	 Work with clean tools in clean surroundings. Remove all outside dirt from housing before exposing bearings. Handle with clean dry hands. Treat a used bearing as carefully as a new one. Use clean solvent and flushing oil. Protect disassembled bearing from dirt and moisture. Keep bearings wrapped in paper or clean cloth while not in use. Clean inside of housing before replacing bearings. Check oil seals and replace as required. Check all plugs and tapped openings to make sure that they are tight. 		
					•				Brinelling of bearing identified by indentation on the ball races, usually caused by incorrectly applied forces in assembling the bearing or by shock loading such as hitting the bearing or drive shaft with a hammer.	When mounting the bearing on the drive shaft use a proper size ring and apply the pressure against the inner ring only. Be sure when mounting a bearing to apply the mounting pressure slowly and evenly.		
					•				False brinelling of bearing identified again by either axial or circumferential indentations usually caused by vibration of the balls between the races in a stationary bearing.	 Correct the source of vibration. Where bearings are oil lubricated and employed in units that may be out of service for extended periods, the drive shaft should be turned over periodically to relubricate all bearing surfaces at intervals of one to three months. 		
					•				Thrust overload on bearing identified by flaking ball path on one side of the outer race or in the case of maximum capacity bearings, may appear as a spalling of the races in the vicinity of the loading slot. (Please note: maximum capacity bearings are not recommended in Mark 2I pumps.) These thrust failures are caused by improper mounting of the bearing or excessive thrust loads.	Follow correct mounting procedures for bearings.		

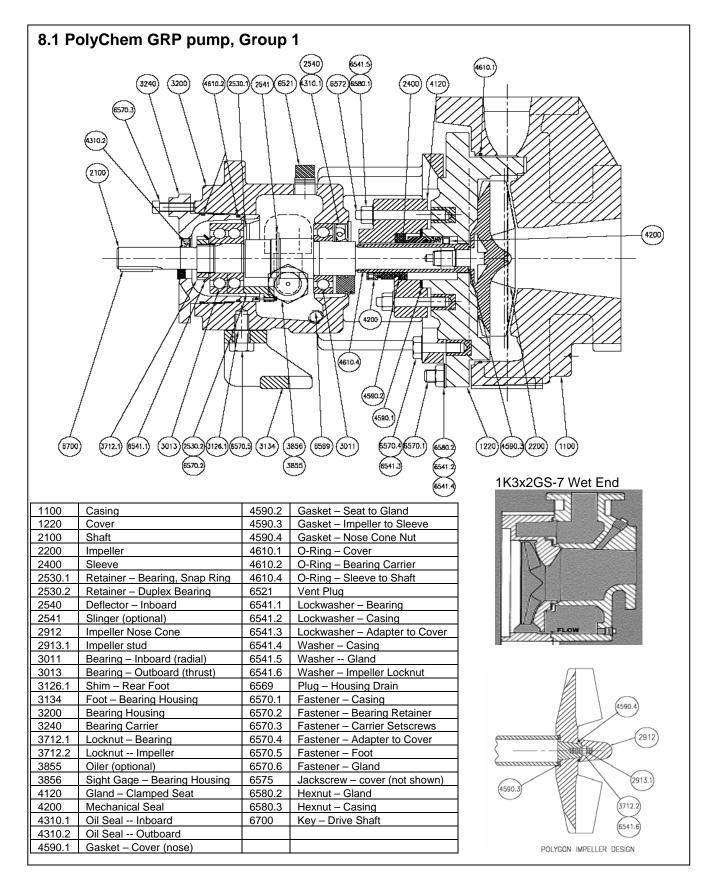


FAULT SYMPTOM

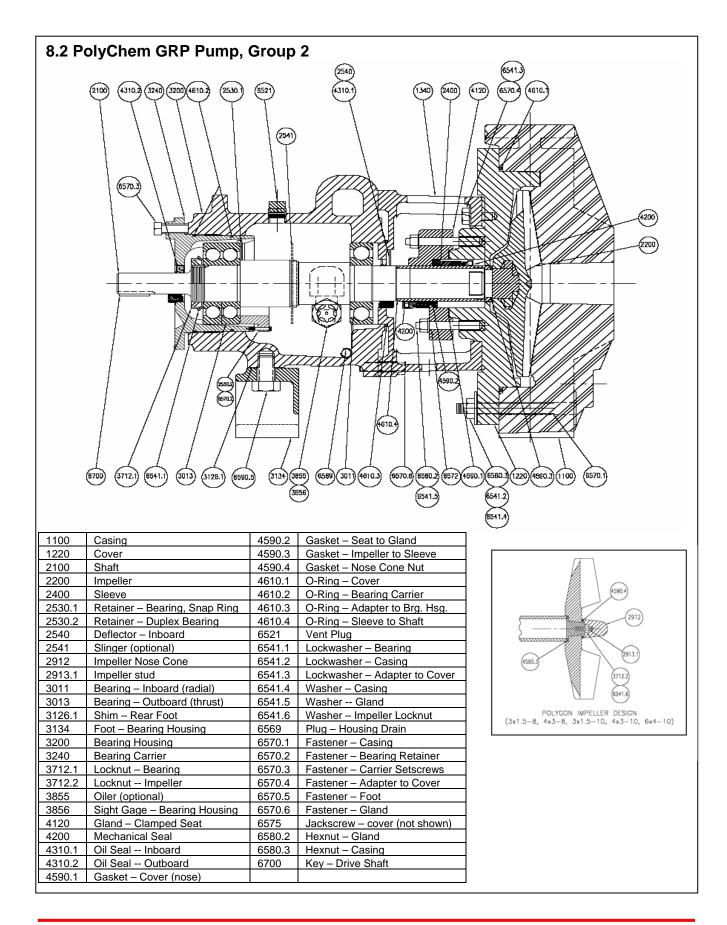
	mp not reaching design flow rate										
₽		· ·	mp not reaching design head (TDH)								
	₽	No	o d	isch	narg	ge o	or fl	low	wit	h pump running	
		₽	Pu	mp	ор	era	tes	s for	r sh	ort period, then loses prime	
			₩	E	kce	ssiv	veı	nois	se fi	rom wet end	
				₩	E	xce	ssi	veı	nois	e from power end	
					₽						
						₽					
							₽				
							Ľ	1			
								ľ	₽	PROBABLE CAUSES	POSSIBLE REMEDIES
					•					Misalignment identified by fracture of ball retainer or a wide ball path on the inner race and a narrower cocked ball path on the outer race. Misalignment is caused by poor mounting practices or defective drive shaft. For example, bearing not square with the centerline or possibly a bent shaft due to improper handling.	Handle parts carefully and follow recommended mounting procedures. Check all parts for proper fit and alignment.
					•					Bearing damaged by electric arcing identified as electro- etching of both inner and outer ring as a pitting or cratering. Electrical arcing is caused by a static electrical charge emanating from belt drives, electrical leakage or short circuiting.	 Where current shunting through the bearing cannot be corrected, a shunt in the form of a slip ring assembly should be incorporated. Check all wiring, insulation and rotor windings to be sure that they are sound and all connections are properly made. Where pumps are belt driven, consider the elimination of static charges by proper grounding or consider belt material that is less generative.
					•					 Bearing damage due to improper lubrication, identified by one or more of the following: 1. Abnormal bearing temperature rise. 2. A stiff cracked grease appearance. 3. A brown or bluish discoloration of the bearing races. 	 Be sure the lubricant is clean. Be sure proper amount of lubricant is used. The constant level oiler supplied with Durco pumps will maintain the proper oil level if it is installed and operating properly. In the case of greased lubricated bearings, be sure that there is space adjacent to the bearing into which it can rid itself of excessive lubricant, otherwise the bearing may overheat and fail prematurely. Be sure the proper grade of lubricant is used.



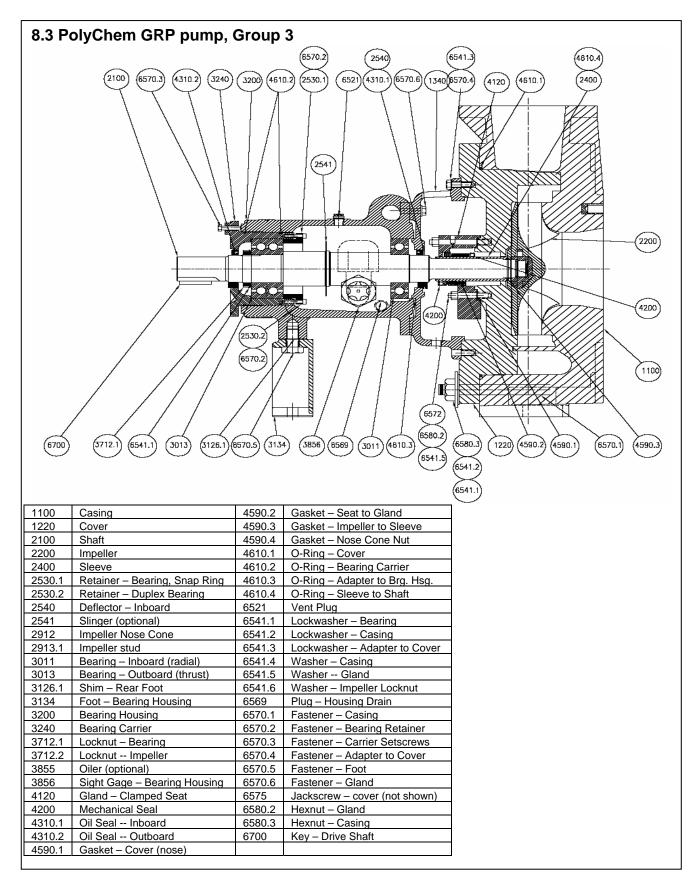
8 PARTS LIST AND DRAWINGS













9 CERTIFICATION

Certificates, determined from the contract requirements, are provided with these instructions where applicable. Examples are certificates for CE marking and ATEX marking etc. If required, copies of other certificates sent separately to the Purchaser should be obtained from Purchaser for retention with these User Instructions.

10 OTHER RELEVANT DOCUMENTATION AND MANUALS

10.1 Supplementary user instructions

Supplementary instructions such as for a driver, instrumentation, controller, seals, sealant systems etc are provided as separate documents in there original format. If further copies of these are required they should be obtained from the supplier for retention with these user instructions.

10.2 Change Notes

If any changes, agreed with Flowserve Pump Division, are made to the product after it is supplied, a record of the details should be maintained with these User Instructions.

10.3 Additional sources of information

The following are excellent sources for additional information on centrifugal pumps in general.

Pump Engineering Manual R.E. Syska, J.R. Birk, Flowserve Corporation, Dayton, Ohio, 1980. Specification for Horizontal End Suction Centrifugal Pumps for Chemical Process, ASME B73.5M The American Society of Mechanical Engineers, New York, NY.

American National Standard for Centrifugal Pumps for Nomenclature, Definitions, Design and Application (ANSI/HI 1.1-1.3) Hydraulic Institute, 9 Sylvan Way, Parsippany, New Jersey 07054-3802.

American National Standard for Centrifugal Pumps for Installation, Operation, and Maintenance (ANSI/HI 1.4) Hydraulic Institute, 9 Sylvan Way, Parsippany, New Jersey 07054-3802.

RESP73H Application of ASME B73.5M-1991, Specification for Horizontal End Suction Centrifugal Pumps for Chemical Process, Process Industries Practices

Construction Industry Institute, The University of Texas at Austin, 3208 Red River Street, Suite 300, Austin, Texas 78705.

Pump Handbook 2nd edition, Igor J. Karassik et al, McGraw-Hill, Inc., New York, NY, 1986.

Centrifugal Pump Sourcebook John W. Dufour and William E. Nelson, McGraw-Hill, Inc., New York, NY, 1993.

Pumping Manual, 9th edition

T.C. Dickenson, Elsevier Advanced Technology, Kidlington, United Kingdom, 1995.





USA and Canada

Flowserve Corporation Pump Division 5215 North O'Connor Blvd, Suite 2300 Irving, TX 75039-5421 USA Telephone: 1 972 443 6500 Toll Free: 1 800 728 PUMP (7867) Fax: 1 972 443 6800

Europe, Middle East & Africa Flowserve Limited

Pump Division Harley House, 94 Hare Lane Claygate, Esher, Surrey KT10 0RB United Kingdom Telephone: +44 (0)1372 463 700 Fax: +44 (0)1372 460 190

Latin America and Caribbean

Flowserve Corporation 6840 Wynnwood Lane Houston, TX 77008 USA Telephone: +1 713 803 4434 Fax: +1 713 803 4497

Asia Pacific

Flowserve Pte Ltd Pump Division 200 Pandan Loop, #06-03/04 Pantech 21, Singapore 128388

Telephone: +65 775 3003 Fax: +65 779 4607

Visit our web site at: www.flowserve.com

Your Flowserve conta	Your Flowserve contact:								
Flowserve Pump Division									
3900 Cook Boulevard									
Chesapeake, VA 2332	3-1626 USA								
Telephone 1 757 4	185 8000								
Fax 1 757 4	185 8149								
Flowserve Pumps Lim PO Box 17, Newark Notts NG24 3EN	nited								
United Kingdom									
Telephone (24 hours)	+44 (0) 1636 494 600								
Sales & Admin Fax +44 (0) 1636 705 99									
Repair & Service Fax	+44 (0) 1636 494 833								
E-mail inewark@flows	erve.com								

Your local Flowserve representative:
To find your local Flowserve representative, please use the Sales Support Locator System found at www.flowserve.com